

ENHANCEMENT OF ANTIFOULING PROPERTIES USING RICE HUSK
SILICA PARTICLES IN POLYSULFONE MEMBRANE AND OPTIMIZATION
OF ITS OPERATING CONDITION

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SPECIAL GRATITUDES TO:

Special for my parent,

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All my friends that give full support,

Person that guide and help me,

Only Allah S.W.T can repay your kindly

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ABSTRACT

This study investigates the effects of rice husk silica (RHS) as additive in the polysulfone membrane to enhance antifouling properties in membrane separation process. The flat sheet PSf/RHS membrane was prepared via phase inversion technique. The characterization and performance test were conducted on PSf ultrafiltration membrane prepared from a different additive concentration. The thermal stability of prepared membrane was observed by using thermogravimetric analysis (TGA). The cross section area and particles distribution of additive were carried out by using the scanning electron microscope (SEM) while the surface morphology was investigated via field emission scanning electron microscope (FESEM). The surface roughness and hydrophilicity were also determined by using Atomic force microscopy (AFM) and contact angle measurement respectively. Meanwhile, the performance was evaluated in term of pure water flux (PWF), rejection and antifouling properties. The optimized of normalized flux (J_f/J_o) at different parameter filtration condition (pH, ionic strength and transmembrane-pressure) was carried out by using the response surface methodology (RSM). From the analysis of SEM, FESEM and AFM, results showed that the microstructure of the membrane especially at top layer and sub layer obviously changed with the incorporation of RHS. The results also demonstrated that the mean pore size was decreased and hydrophilicity was increased as increased RHS particles in PSf membrane. The performance of the membrane was analyzed by using distilled water for permeation test and humic acid for the rejection test. The results also showed that the hydrophilic PSf/RHS membrane has significantly improved the permeation and rejection performance after the addition of RHS. The results showed that the addition of 4 wt. % RHS give the highest flux at 300.50 L/m².hour (LMH). The highest rejection was found at 3 wt. % of RHS membrane with value 98% for UV₂₅₄ and 96% for TOC. The optimal value of J_f/J_o was found at 0.62 with the parameter condition pH: 6.10, ionic strength: 0.05 mol/L and transmembrane-pressure: 2.67 bars. Optimize of RSM analysis also proved that the error of model is less than 0.05% which indicates that the model is significant.

ABSTRAK

Kajian ini menyiasat kesan silika sekam padi (RHS) sebagai bahan tambah dalam membran polisulfon untuk ciri-ciri anti-kekotoran di dalam proses pemisahan membran. Lembaran rata daripada membran PSf/ RHS telah disediakan melalui teknik fasa balikan. Pencirian dan ujian prestasi telah dijalankan ke atas penapisan ultra membran yang disediakan daripada kandungan RHS yang berbeza. Kestabilan terma membran dikaji dengan menggunakan analisis Termogravimetri (TGA). Kajian ke atas keratan rentas dan taburan zarah pada membran telah dijalankan dengan menggunakan mikroskop imbasan elektron (SEM) manakala morfologi permukaan telah disiasat melalui bidang pelepasan mikroskop imbasan elektron (FESEM). Kekasaran permukaan dan sifat hidrofilik juga ditentukan melalui daya Atom mikroskopi (AFM) dan ukuran sudut sentuh. Sementara itu, prestasi aliran air tulen (PWF), penolakan dan pencirian anti-kekotoran juga dijalankan. Proses mengoptimumkan fluks normal (J_f / J_o) pada keadaan penapisan yang berbeza parameter (pH, kekuatan ionik dan membran tekanan membran) telah dijalankan dengan menggunakan kaedah gerak balas permukaan. Keputusan yang ditunjukkan oleh SEM, FESEM dan AFM bahawa mikrostruktur membran terutama di lapisan atas dan lapisan sub telah berubah. Keputusan kajian juga menunjukkan bahawa saiz purata liang menurun dan peningkatan sifat hidrofilik meningkat disebabkan peningkatan kuantiti RHS dalam membran PSf. Prestasi membran dianalisa dengan menggunakan air suling untuk ujian penyerapan dan asid humik untuk ujian penolakan. Keputusan juga menunjukkan bahawa membran prestasi penyerapan dan penolakan PSf/RHS hidrofilik telah meningkat selepas penambahan RHS. Hasil kajian menunjukkan bahawa dengan tambahan 4 wt. % daripada RHS memberi fluks tertinggi iaitu 300.50 L/m².jam (LMH). Penolakan tertinggi ditemui dengan 3 wt. % daripada RHS membran dengan nilai 98% untuk UV₂₅₄ dan 96% untuk TOC . Nilai optimum J_f / J_o ditemui pada nilai 0.62 dengan keadaan parameter pH: 6.1, kekuatan ionik 0.05 mol/L dan tekanan membran: 2.67 bar. Analisa optimum dengan menggunakan RSM juga membuktikan bahawa ralat model adalah kurang daripada 0.05% dan menunjukkan bahawa model adalah boleh diterima pakai.

TABLE OF CONTENTS

DESCRIPTION	PAGE
TITLE	i
DECLARATION	ii
DEDICATION	iv
ACKNOWLEDGEMENT	v
ABSTRACT	vi
ABSTRAK	vii
CONTENTS	viii
LIST OF TABLES	xiii
LIST OF FIGURES	xiv
LIST OF ABBREVIATIONS	xvi
LIST OF APPENDIXES	xviii
 CHAPTER 1	
INTRODUCTION	1
1.1 Introduction	1
1.2 Problem Statement	3
1.3 Research Objectives	4
1.4 Research Scope	4
 CHAPTER 2	
LITERATURE REVIEW	6
2.1 Introduction	6
2.2 Membrane separation processes	6
2.3 Membrane process	8
2.4 Types of Membrane	10
2.5 Polysulfone membrane	11
2.6 Membrane formation	12

2.6.1	Phase inversion	12
2.6.2	Immersion precipitation	14
2.7	Membrane fouling mechanism	15
2.7.1	Fouling characteristic	15
2.7.2	The effect in membrane fouling	16
2.7.2.1	Effect of pH	17
2.7.2.2	Effect of ionic strength	17
2.7.2.3	Effect of concentration	18
2.7.2.4	Effect of Transmembranepressure	18
2.8	Enhancement of antifouling properties	19
2.8.1	Effect of additive in membrane modification	19
2.8.1.1	Effect of polymer additive	20
2.8.1.2	Effect of inorganic additive	21
2.9	Response Surface Methodology (RSM)	23

CHAPTER 3 METHODOLOGY 25

3.1	Introduction	25
3.2	Membrane materials	27
3.2.1	Polymer selection	27
3.2.2	Solvent	28
3.2.3	Additive	29
3.2.3.1	Polymer additive	29
3.2.3.2	Inorganic additive	30
3.3	Membrane fabrication	33
3.4	Characterization	33
3.4.1	X-ray Diffraction (XRD)	33
3.4.2	Fourier transforms infrared spectroscopy (FTIR)	33
3.4.3	Scanning electron microscope (SEM) and Energy-dispersive X-ray spectroscopy analysis (EDX)	34

3.4.4	Thermogravimetric analysis (TGA)	35
3.4.5	Field Emission Scanning Electron Microscope (FESEM)	35
3.4.6	Atomic force microscopy (AFM)	35
3.4.7	Contact angle	36
3.4.8	Tensile test	36
3.4.9	Porosity and mean pore size	36
3.5	Membrane performance evaluation	37
3.5.1	Preparation of Humic acid (HA)	38
3.5.2	Membrane performance rejection Testing (UV ₂₅₄) spectrometer	39
3.5.3	Analysis of the total organic carbon (TOC)	39
3.5.4	Calculation of Pure Water Flux (PWF) and humic acid rejection	40
3.6	Membrane fouling analysis	40
3.7	Optimization on effect of operating condition on membrane fouling	42
3.7.1	Factorial design (first order model)	42
3.7.2	Second Order Model (Response Surface Methodology)	42
3.7.3	Analysis of variance (ANOVA)	44
3.7.4	Optimization process	44
3.7.5	Confirmation test	45

CHAPTER 4 RESULT AND DISCUSSION 46

4.1	Introduction	46
4.2	Characterization of rice husk silica as inorganic additive	47
4.2	Characterization of RHS loading in polysulfone (PSf) membrane	49
4.2.1	FTIR analysis	49
4.2.2	Effect of RHS loading in thermal	

	properties of membrane	50
4.2.3	Contact angle analysis	52
4.2.4	Membrane morphology	53
	4.2.4.1 Cross section area and Membrane surface	53
	4.2.4.2 Particles distribution (EDX analysis)	57
	4.2.4.3 AFM analysis	59
4.2.5	Porosity (ϵ) and tensile strength	61
4.2.6	Mean pore size	63
4.3	Performance of RHS membrane	64
	4.3.1 Pure water flux	64
	4.3.2 Rejection	65
4.4	Fouling analysis	67
	4.4.1 Anti-fouling performance	67
	4.4.2 Individual resistance	69
4.5	Study on effect of operating condition on RHS membrane fouling	71
	4.5.1 First Order Model - Factorial design	71
	4.5.1.1 ANOVA analysis and analysis Normal Probability	72
	4.5.2 Second Order Model- Response Surface Methodology (RSM)	74
	4.5.2.1 ANOVA analysis	74
	4.5.2.2 Effect of pH, Ionic strength (IO) and Tranpresure membrane (TPM) on normalized flux (J_f / J_o)	78
	4.5.2.2.1 Effect of Trans- Pressure Membrane (TMP)	82
	4.5.2.2.2 Effect of pH	83

4.5.2.2.3	Effect of ionic strength (IO)	85
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4.5.3	Optimization and Verification of the normalized flux (J_f/J_o)	86
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CHAPTER 5	CONCLUSION	88
------------------	-------------------	-----------

5.1	Conclusion	88
-----	------------	----

5.2	Recommendations	89
-----	-----------------	----

REFERENCES	91
-------------------	-----------

APPENDICES	102
-------------------	------------



LIST OF TABLES

2.1	Cross flow membranes process	9
3.1	The properties of PSf UDEL 170	28
3.2	The properties of NMP	29
3.3	The properties of PEG	30
3.4	The dope formulation in membrane fabrication	33
3.5	Ranges of parameters based on previous studies	42
3.6	The coded value of second order model	43
4.1	The mass of Si element in membrane	58
4.2	Average membrane surface roughness via AFM	60
4.3	Average pore size of membrane	63
4.4	Fluxes of the membrane during humic acid filtration process	68
4.5	The result experimental layout of 2^3 full factorial CCD	71
4.6	ANOVA for 2^3 full factorial design: response	73
4.7	Full Factorial design (Second Order Model)	76
4.8	ANOVA analysis for RSM Quadratic Model	77
4.9	Comparison between the prediction value and actual value	87

LIST OF FIGURES

2.1	Two phase system separated by membranes	7
2.2	Chemical structure of polysulfone (PSf) polymer	11
2.3	Schematic of the immersion precipitation process	14
2.4	Types of membrane fouling mechanism	16
3.1	The flow chart of methodology	26
3.2	N-Methyl-2 Pyrrolidone (NMP) molecular structure	29
3.3	Rice husk	30
3.4	Instrument for dope sample preparation	31
3.5	The flat sheet membrane preparation by using phase inversion method	32
3.6	Scanning Electron Microscope (JEOL JSM-6380LA)	34
3.7	Schematic of permeation testing unit	38
3.8	The size of humic acid distribution by intensity	39
4.1	XRD analysis of RHS particles	47
4.2	The EDX analysis of RHS particles	48
4.3	The RHS size distribution by intensity	48
4.4	ATR-FTIR analysis	50
4.5	Thermo gravimetric curves of pristine and modified membrane	51
4.6	Contact angle analysis	52
4.7	Diagram of Asymmetric structure of prepared membrane	53
4.8	Morphology of PSf membrane	55
4.9	EDX result of Si element on the surface modified membrane	57
4.10	EDX result of Si element on the cross section of modified membrane	58
4.11	AFM images for RHS with different	

	concentration of RHS	60
4.12	Tensile strength and porosity	63
4.13	Permeation water flux	65
4.14	Rejection graph of TOC and UV_{254}	66
4.15	Normalized flux	68
4.16	The individual filtration resistance of membrane	70
4.17	Normal plot of residuals	73
4.18	The normal plot residuals for second order model	77
4.19	The three-dimensional response surface and contour plot	80
4.20	Interaction plots of J_f/J_o on pH, IO and TPM	81
4.21	Normalized flux at Run 16, 17 and 18	82
4.22	The normalized flux at Run 13, 12 and 19	84
4.23	a) solution at low pH. b) solution at high pH	84
4.24	Normalized Flux of Run 14, 15 and 18	85
4.25	The optimal prediction condition of J_f/J_o response	86



LIST OF ABBREVIATIONS

AFM	Atomic Force Microscopy
ASTM	American Society for Testing and Materials
A	Membrane Area (m^2)
C_p	Solute Concentration in permeate stream
C_f	Solute Concentration in Feed
CA	Cellulose Acetate
FTIR	Fourier transform-infrared
FESEM	Field Emission Scanning electron microscopy
HA	Humic Acid
J_{wf}	Total of pure water flux
J_{cp}	Total of filtration
J_c	Total of pure water flux after physical cleaning
J_a	Total of pure water flux after chemical cleaning
J_o	Pure Water Flux of clean Membrane
J_f	Pure Water Flux of Fouled Membrane
J_f/J_o	Normalizes flux (initial flux / final flux)
LMH	$L/m^2 \cdot h$
MD	Membrane Distillation
MF	Microfiltration
NF	Nanofiltration
NMP	N-methyl-2-pyrrolidone
PEG	Polyethylene glycol
PWF	Pure Water Flux
PSf	Polysulfone
Q	Permeate volume (L)
R	Rejection of feed components
R_t	Total resistance

R_m	Membrane resistance
R_a	Resistance due to absorption
R_c	Resistance due to cake layer
R_{cp}	Resistance due to cake polarization
RHS	Rice husk silica
RSM	Response surface methodology
RO	Reverse osmosis
SEM	Scanning electron microscope
SiO_2	Silica Oxide
UF	Ultrafiltration
Wt. %	Weight Percentage
XRD	X-ray diffraction
Δt	Time (h)



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LIST OF APPENDICES

APPENDIX	TITLE	PAGES
A	List of publications and awards	102
B	The material and instrument used in Membrane characterization	103
C	Result of Energy-dispersive X-ray Spectroscopy analysis (EDX)	107
D	Calibration result	108
E	Overall flux rate in filtration of prepared membrane	108



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CHAPTER 1

INTRODUCTION

1.1 Introduction

In recent years, water pollution has become a serious issue that need to be discussed and attract attention from all over the world. Based on World Health Organization society, the worst situation that facing by most people in the world is the lack of access to get clean water. As the world population is going to be increased to 1.1 billion by year 2015, the contamination problem from all sources of clean water i.e. river water, rain water, sea, lake are with unwanted material such as bacteria, floating debris and dust is becoming a serious problem that need to be handled (Tebbutt *et al.*, 1998). Thus, many researches have been conducted recently to treat the water medium via different approaches such as activated carbon, activated alumina, aeration, ion exchange, neutralizing filter and membrane. Based on extensive study that reported in source articles, membrane technology offer much easiest way.

Basically, a membrane is divided into several types of separation such as microfiltration, ultrafiltration, nanofiltration and reverse osmosis. Ultrafiltration can be used to remove contaminants from the polluted water with the intense regulatory activity and scarce high quality source water. These stages of separation can be considered as a very promising process for drinking water production due to its pore sizes range that is between 2 - 100 nm. Ultrafiltration is able to remove viruses, bacteria, colloids, and larger particulate matter from suspensions (Dorgan, 1992). According to Haijun *et al.*, (2009) polysulfone (PSf) is a very popular polymer and widely used in the fabrication of ultrafiltration membrane due to its good mechanical, thermal and chemical stability. However, because of its hydrophobic nature, PSf membranes are susceptible to membrane fouling by the adsorption of proteins and other biomolecules from the feed stream (Yan, Xiang, and S. Xianda, 2006). This

fouling mechanism causes the flux decline by concentration polarization where a membrane undergoes plugging or coating by some element in the stream being treated, in such a way its output or flux is reduced. In general, when fouling occurs in separation process it can affect the performance of membrane such as flux permeation, water permeability, surface porosity and morphological (Mansourizadeh and Ismail, 2010).

Most previous studies have shown that incorporation of additive into membrane formulation can play an important role in preventing the fouling problem which may cause improper morphology structure including its pore and skin layer (Vatanpour *et al*, 2011; Nghiem *et al.*, 2008). The incorporation of different material or additive have contribute to significant effect to membrane performance by reducing fouling and increasing rejection. The incorporation of additives in membrane formation is expected to add value to membrane properties to make porous, increase hydrophilicity, induced antibacterial properties and enhanced membrane performances (Saljoughi *et al*, 2010; B.Torrestinana-Sancheza *et al.*, 1998; Basri *et al.*, 2010). The incorporation of most inorganic fillers such as polymeric additive, silica, aluminum, zeolite, and titanium dioxide to dope solutions is able to produce membranes with higher porosity and hydrophilicity (Ma *et al*, 2011; Idris *et al.*, 2011; Jian *et al.*, 2012 and Arthanareeswaran *et al.*, 2007).

The potential of organic fibers from natural sources (non-hazardous element) for example rice husk (which has high silica content) was being considered due to its biodegradable properties and green technology. In fact, some inorganic additives are able to suppress the formation of macrovoids, enhance pore formation and improve pore interconnectivity and hydrophilicity of the membranes. The inorganic additive also can increase membrane permeability and control membrane surface properties (Chakrabarty *et al*, 2008). As reported by Yan *et al.*, the additive of aluminum oxide (inorganic) used as additive in membrane dope formulation has improved the antifouling properties (Yan *et al.*, 2007). By improving membrane hydrophilicity it can reduce the membrane fouling to some extent.

The addition of additive in membrane formulation is expected to change the characteristic such as pore sizes, pore distribution, physical properties and mechanical characteristic. As reported in many papers, silica can suppress the formation of amphiphilic component and macrovoids, enhance the pore formation, improve pore interconnectivity and hydrophilicity for the membrane (He *et al*, 2002;

Qu *et al.*, 2010; Hero *et al.*, 2006; Huang *et al.*, 2012 and Arthanareeswaran *et al.*, 2007). The incorporation of potential organic fibres from natural sources (non-hazardous element) i.e. rice husk was considered as its contain high silica compound. Besides that it also has biodegradable properties and offers green technology. Hopefully, the incorporation of this additive will improve the antifouling mechanism of the membrane and membrane performance at the same time reduces the costs.

1.2 Problem Statement

Most applications in membrane separation process i.e. chemical, food, petroleum, mining etc. having a critical problem with fouling mechanism. Membrane fouling is characterized in general as a reduction of permeate flux through the membrane, as a result of increased flow resistance due to pore blocking, concentration polarization, cake formation and absorption. Membrane fouling gives a negative impact on filtration performance as it decreases the permeate flux or increases the transmembrane-pressure (TMP). The effect of this fouling mechanism on the decrease of flux depends on factor such as membrane pore size, solute loading and pore size distribution, membrane material and operating conditions. In addition, the efficiency of membrane separation process is highly dependent on fouling effect of natural organic matter (NOM) that present in surface water. Humic substance is a major component in NOM and generally categorized into humic acid (HA) (Combe *et al.*, 1999). Al-Amoudi reported that pH and ionic strength affect the molecular size distribution of HA (Al-Amoudi, 2010). This NOM can change the molecule to be large, flexible and linear shape at high and low pH (Al-Amoudi, 2010). In addition, the high ionic strength and concentration in HA water also accelerate the fouling formation on membrane (Wang *et al.*, 2001). Thus it is necessary to study the anti-fouling mechanism of membrane in membrane separation process. The good and potential additive which can enhance the antifouling performance will be determined. The addition of suitable additive is wisely needed in order to modify membrane structure and properties to overcome this fouling phenomena. The modification of suitable additive in membrane formulation will be carried out and the effect of membrane properties and structure will be investigated. Silica from rice husk is highly potential as additive that induced hydrophilicity properties can enhance the antifouling agent.

1.3 Research Objectives

The objective of this work were:

- i. To prepare ultrafiltration composite membrane with silica from rice husk as an additive at different weight percentage.
- ii. To study the effect of rice husk silica (RHS) as additive towards polysulfone (PSf) membrane characteristic and performance.
- iii. To determine the fouling properties of prepared membrane.
- iv. To optimize normalized flux of PSf/RHS membrane at three difference parameter filtration such as pH, ionic strength and transmembrane-pressure by using response surface modeling (RSM).

1.4 Research Scope

In order to achieve the above mentioned objectives, the following scopes of study were drawn.

- i. Preparing the silica from rice husk at burning temperature 600 °C as an additive and characterize in term of XRD pattern, particles content and size of particles.
- ii. Fabricating composite membrane by preparing dope solutions from PSf as polymer material, N-Methyl-2-pyrrolidone (NMP) as solvent, PEG 400 as pore forming agent and RHS as additive at different concentration (0 – 6 wt. %) via phase inversion technique.
- iii. Characterizing the prepared membrane in terms of its cross section area, surface morphology, surface roughness, particles distribution, hydrophilicity, porosity, mean pore sizes and tensile strength.
- iv. Measuring performance of prepared the membrane via pure water flux (PWF) and rejection of humic acid (HA) solution by using ultrafiltration permeation testing unit.
- v. Evaluating fouling performance filtration of HA by using the ultrafiltration permeation testing unit in term of membrane resistance, normalized flux, and flux recovery after membrane chemical and physical cleaning.

- v. Optimizing of PSf/RHS membrane performance on final normalized flux at three difference operating condition (pH, Ionic strength and transmembrane-pressure by using Response Surface Methodology (RSM).

1.5 Research significance

Due to the nature of current polysulfone membranes that has hydrophobic properties and tends to absorb foulants at top and inside the pore structure, therefore the enhancement of membrane to increase antifouling properties is crucially needed. In this study, the use of silica that poseses strong hydrophilicity had proven can increase membrane structure and performance. In fact, the synthesization of silica from agro waste material which is rice husk not only can minimize the pollution but also introduce green materials to membrane technology. Furthermore, the use of RSM also provides the variable response in getting the optimized range of filtration operation which benefit to membrane technology



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CHAPTER 2

LITERATURE REVIEW

2.1 Introduction

This chapter will discuss on previous related works on the membrane separation process. This section will explain the effect of fouling towards membrane performance. Further explanation on membrane modification and fabrication will also be highlighted.

2.2 Membrane Separation Process

Membrane separation can be defined as the filtration of two or more components from a fluid stream based on size difference (Munir, 2000). According to Mulder the definition of membrane is a selective barrier between two phases (Marcel Mulder, 1991). The term 'selective' being inherent to a membrane or a membrane process. Membrane separation describes the ability of a membrane to control the permeation rate of particles and molecules passing through the membrane. The membrane has the ability to transport one component more readily than the other because of differences in physical or chemical properties between the membrane and the permeating components. The movements of those components across the membrane need a driving force. Figure 2.1 shows the schematic diagram of membrane separation concept. The diagram demonstrated that phase 1 is that usually considered as feed or upstream side while phase 2 is considered as permeates or downstream side (Marcel Mulder, 1991). The solute bigger particle has tendency to foulant and blocked the inner pore, meanwhile the smaller particle will pass through the membrane which is called permeates. The concentration bigger particle of blocked by the membrane calculated to get rejection data.

Nowadays, membrane widely used in river water filtration, waste water treatment, desalination of sea water, purification of food, gas separation, pharmaceutical product and etc. Hence, membranes are developed individually in different industrial field in order to fulfill the current needs. In membrane fabrication, there are two factors that determine the performance of a membrane separation process; selectivity and productivity. Selectivity is expressed as a parameter called retention or separation factor. Productivity is expressed as a parameter called flux (Marcel Mulder, 1991). However, membrane fouling is one of constrain in membrane separation and give negative effect on membrane performance.

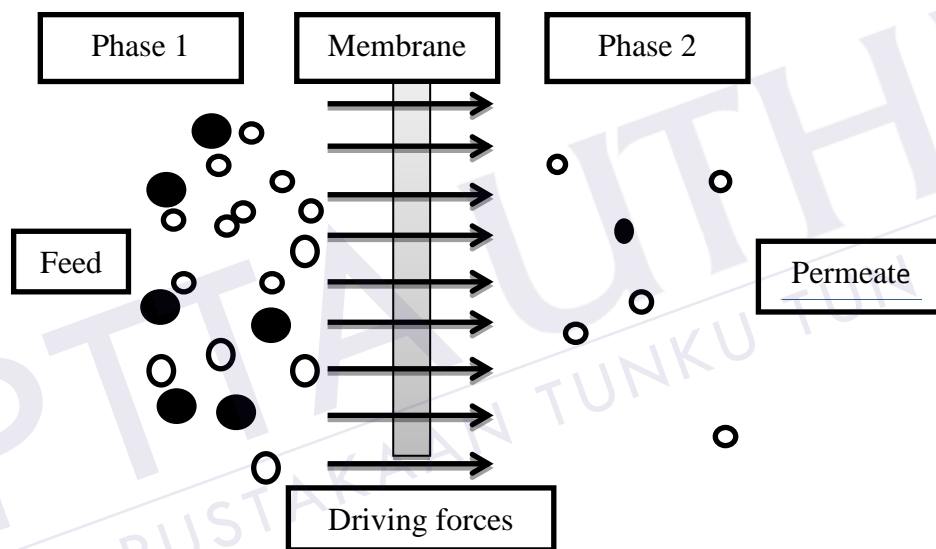


Figure 2.1: Two phase system separated by membranes (Mulder, 1991).

2.3 Membrane process

Membrane is the important element in every membrane separation process. It can be considered as a perm selective barrier of interface between two phases. Separation happens due to the ability of membrane to transfer one or more selected component of the feed mixture to permeate. Membrane filtration which is classified into microfiltration (MF), ultrafiltration (UF), nanofiltration (NF) and reverse osmosis (RO) is a pressure process. Table 2.1 discusses a different membrane process between ultrafiltration (UF), nanofiltration (NF) microfiltration (MF) and reverse osmosis (RO). The process difference depending on the component retained, trans-membrane pressure and process application.

In this study, ultrafiltration (UF) is typically used to separate macromolecules and colloids from a solution, e.g. water or micro-solutes. The average pore size of the membranes used is in the 2-100 nm range. In general, UF has been used in a wide field of applications such as food and dairy industry, pharmaceutical and biotechnology industry, textile industry, chemical industry and so on. UF is a pressure driven process, freely permeable to the solvent but impermeable to the concentrated solutes (Yanlei *et al*, 2008). The solvent molecules flow through the membrane pores and can be collected on the downstream side of the system.

In addition, UF processes are also used to remove low molecular weight materials from solutions, such as in the desalting of macromolecular solutions. UF membranes are also used to fractionate different sized molecular species, by virtue of the fact that these membranes have very well defined pore diameter distributions. UF membranes are available in a variety of configurations, the operating pressures of 2 to 9 bars are usual and its water fluxes vary widely, but can be as high as 5000 L/m²h in some systems (Marcel Mulder, 1991 and Wang *et al.*, 2006).

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