

STUDY ON THE GAS PERFORMANCE OF CERAMIC MEMBRANE FROM
KAOLIN PREPARED BY PHASE INVERSION TECHNIQUE

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Special dedication to:

My Beloved Father, Mr Hubadillah Hj Mohamed

My Beloved Mother, Mrs Rosnah Bt Hashim

and

For Beloved Siblings,

Madam Siti Aminah Bt Hubadillah

Kapten Ibrahim Bin Hubadillah

Dr. Siti Fatimah Bt Hubadillah

Prof. Mohamed Ismail Bin Hubadillah

and

My intelligent friend, Nurul Nadia aka Alya

I love you all....



PTTA UTHM
PERPUSTAKAAN TUNKU TUN AMINAH

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ABSTRACT

Membrane for gas application have been widely used. Apart from that, ceramic membrane is gaining much attention towards separation technology due to its characteristics of offering high mechanical strength, chemical resistivity and thermal compatibility. However, production of ceramic membrane for gas separation in term of cost and energy reduce still remains as challenge until now, therefore this work addressed to the development of ceramic membrane from kaolin via simple phase inversion technique. First, ceramic membrane suspension have been prepared by stirring kaolin as raw material, N-methyl-2-pyrrolidone (NMP) as solvent and polyethersulfone (PESf) as binder. Phase inversion technique conducted by casted the suspension on the glass plate with casting knife. In order to achieve the aims of this study, the development of ceramic membrane from kaolin were conducted into two objectives: (1) effect of particles sizes and, (2) effect of non-solvent coagulant bath. The types of kaolin particle sizes devoted as Type A kaolin (0.4-0.6 μ m) and Type B kaolin (10-15 μ m) whereas for different types of non-solvent were distilled water, ethanol and mixture of 70% NMP and 30% distilled water. Overall analysis showed that both effect of particle size and different coagulant generated different structure, properties and characteristic of membrane at two different composition. Polymer phase inversion is dominated at kaolin content of 24 to 34wt.% that caused the formation of finger-like voids of the phase inversed structure with Type A kaolin and strong coagulant of distilled water. An opposed condition was shown at highest kaolin content of 39 wt.% for both parameter that can be correlated to the viscous fingering mechanism in the formation of ceramic membrane structure. A slightly similar results trends and pattern was demonstrated with Type B kaolin and weakest coagulant (mixture of 70% NMP and 30% distilled water). Overall performance showed that membrane with Type A kaolin and immersed into ethanol as coagulant at kaolin content of 39 wt.% showed the highest rejection (5.49 and 5.82 for CO₂/N₂ and O₂/N₂, respectively).

ABSTRAK

Membran bagi aplikasi gas telah digunakan secara meluas. Selain itu, membran seramik mendapat banyak perhatian terhadap teknologi pemisahan kerana ciri-cirinya dalam menawarkan kekuatan mekanikal yang tinggi, rintangan kimia dan keserasian terma. Walau bagaimanapun, pengeluaran membran seramik untuk pemisahan gas dari segi kos dan tenaga masih kekal sebagai cabaran sehingga sekarang, oleh itu kerja-kerja ini ditujukan kepada pembangunan membran seramik dari kaolin melalui teknik fasa penyongsangan mudah. Pertama, membran seramik telah disediakan dengan teknik kacau daripada kaolin sebagai bahan mentah, N-methyl-2-pyrrolidone (NMP) sebagai pelarut dan polyethersulfone (PESf) sebagai pengikat. Teknik fasa penyongsangan dijalankan pada plat kaca dimana membrane dibentuk oleh pisau pembentuk. Untuk mencapai matlamat kajian ini, pembangunan membran seramik dari kaolin telah dijalankan kepada dua matlamat: (1) kesan zarah saiz dan, (2) kesan mandi koagulan bukan pelarut. Jenis-jenis saiz kaolin dikhaskan sebagai Jenis A kaolin (0.4-0.6 μ m) dan Jenis B kaolin (10-15 μ m) manakala bagi jenis bukan pelarut ialah air suling, etanol dan campuran 70% NMP dan 30% air suling. Analisis keseluruhan menunjukkan bahawa kedua-dua kesan saiz zarah dan koagulan berbeza menghasilkan struktur berbeza, sifat-sifat dan ciri-ciri membran daripada dua komposisi yang berbeza. Fasa polimer penyongsangan dikuasai pada kandungan kaolin daripada 24 hingga 34wt.% Yang menyebabkan pembentukan lompong jari daripada kaolin Jenis A dan koagulan kuat air suling. Keadaan bertentangan ditunjukkan pada kandungan kaolin tertinggi 39 wt.% Untuk kedua-dua parameter yang boleh dikaitkan dengan mekanisma jari likat dalam pembentukan struktur membran seramik. Trend yang sama telah dihasilkan oleh membran daripada kaolin Jenis B kaolin dan koagulan paling lemah (campuran 70% NMP dan 30% air suling). Prestasi keseluruhan menunjukkan bahawa membran dengan kaolin Jenis A dan etanol sebagai koagulan di kandungan kaolin 39 wt.% menunjukkan gas penolakan yang paling tinggi (5.49 dan 5.82 untuk CO₂ / N₂ dan O₂ / N₂).

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LIST OF ABBREVIATIONS

AFM	- Atomic Force Microscopy
Al	- Aluminum
Al ₂ O ₃	- Alumina Oxide
BSCF	- Ba _{0.5} Sr _{0.5} Co _{0.8} Fe _{0.2} O _{3-δ}
CH ₄	- Methane
CO ₂	- Carbon Dioxide
FESEM	- Field Emission Scanning Electron Microscopy
FTIR	- Fourier Transform Infrared Spectroscopy
MF	- Microfiltration
MIP	- Mercury Intrusion Porosimetry
N ₂	- Nitrogen
NF	- Nanofiltration
Ni	- Nickel
NiO	- Nickel (II) Oxide
NMP	- N-methylpyrrolidone
O	- Oxide
O ₂	- Oxygen
PESf	- Polyethersulfone
PSA	- Particle Size Analysis
PSD	- Pore Size Distribution
PVDF	- Polyvinylidenedifluoride
RO	- Reverse Osmosis
SEM	- Scanning Electron Microscopy
Si	- Silica
SiO ₂	- Silica (II) Oxide
SOFc	- Solid Oxide Fuel Cell
ZrO ₂	- Zirconia Oxide

LIST OF SYMBOLS

σ_b	-	Mechanical Strength
R_a	-	Surface Roughness
F	-	Fracture Force
L	-	Membrane Span Length
w	-	Membrane Width
t	-	Membrane Thickness
P	-	Gas Permeability
Q	-	Flowrate
A	-	Membrane Area
Δ_p	-	Pressure Gradient



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CHAPTER 1

INTRODUCTION

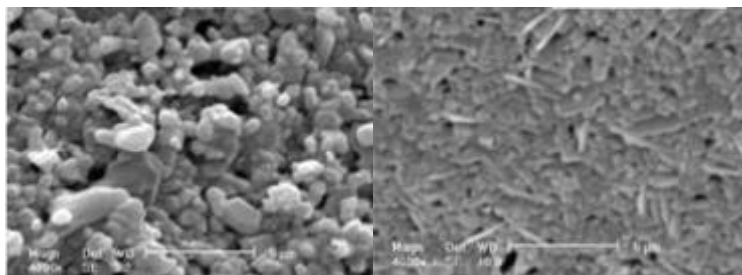
1.1 Background of Study

The impact of global warming caused by discharges of CO₂ from various sources is a major worry. According to the Environmental Protection Agency, the U.S. emitted 6,673 million metric tons of CO₂ into the atmosphere in 2013 [1]. The escalating level of atmospheric CO₂ has caused widespread public concern [2]. One of the major sources of CO₂ emission is fossil fuel combustion. Today, coal-fired power plants alone emit about 2 billion tons of CO₂ per year [3]. Imagine for another 30 years, fossil fuels will remain an important source of the world's energy. For instance, high indoor levels of CO₂ could lead to severe health effects, even death. In fact, carbon dioxide level is allowed to be at the 5% level or 600 ppm [4] in normal environment. The exceed value will help increase a poisonous quality which harm to health. A recent data from Intergovernmental panel on climate change in 2014 reveal that the CO₂ concentration has reached 394ppm [5] in the atmosphere which is far beyond the upper safety limit of 350ppm [6]. Hence, separation of CO₂ removal is crucially required for most of industry actions to avoid excessive CO₂ gas pollution. Other than CO₂, the separation of oxygen from nitrogen in the air also is an important procedure that is widely used in manufacturing. Oxygen is utilized to give advantages in various chemical processes such as natural gas combustion, coal gasification, sewage treatment and welding. Whilst, nitrogen used as a low-temperature coolant, an inert diluent and in the production of ammonia.

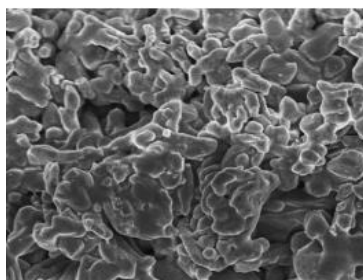
There are various method used in gas separation technology such as cryogenic distillation, pressure swing adsorption and liquid solvent absorption have been proposed. However, the cost associated with the above mentioned processes are about 80% of the total cost of CO₂ sequestration and thus are not fiscally viable. Membranes

offer a promising separation technology to execute process intensification strategies, that is the cutback of production costs by minimizing equipment size, energy consumption and waste production [7]. Apart from that, there are two types of membrane: (1) polymeric membrane and (2) inorganic membrane. Polymeric membranes are widely used among all types of membranes. This has, in accordance of polymeric membranes offered a cheaper method, and yet the simple fabrication process involved. However, it is well known challenges of low selectivity and permeability in polymer membranes which have been addressed with some degree of success with advanced engineering polymers [7]. Furthermore, the physical and properties of polymer which cannot endure the application requiring high thermal, chemical and strength has limit the application of polymer membrane for critical applications. Because of this, researchers have taken attention towards inorganic membranes that has the ability to sustain at high temperature and extreme condition. In general, ceramic membrane can be subdivided into another three types: (1) ceramic membrane, (2) metal membrane and, (3) carbon membrane. The latest development has shown that ceramic membrane is gaining a place in gas separation compared to other membranes as it is offer simple sieving mechanism through the pore size obtained [8]. Since ceramic membranes offer significant advantages over polymeric membranes, therefore, it has been widely used especially in oilywater separation [9], wastewater separation [10] and water separation [11]. However, for the past few years the application of ceramic membrane still dominated the application in many gas industries which demanded high thermal and pressure.

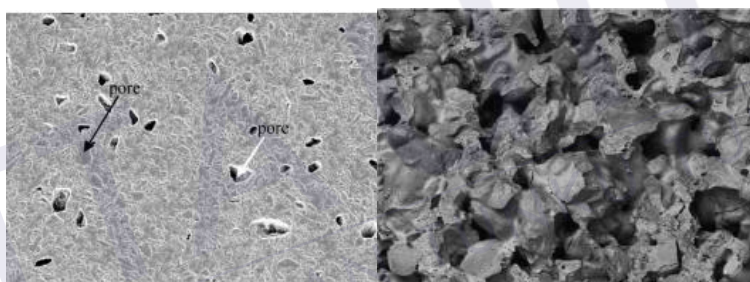
There are sundry unique structure could be obtained in ceramic membrane fabricated at different method as shown in Figure 1.1. In gas application, each type of dense membrane structure could be applied according to felicitous gas application based on their pore size and surface properties in order to have a high selectivity and a low permeation rate. The ability of ceramic membranes could be produced or fabricated towards desired structure such as dense or porous membranes has attracted intensive study of ceramic membrane development and modification such as high temperature, highly acidic or basic feed [12-14]. For instance, the past decade has witnessed major changes in this area as dense ceramic membranes exhibiting high oxygen ionic and electronic conductivity have become of greatest interest as it is economical, clear and effective way of producing oxygen by separation from air or other oxygen containing gas mixtures.



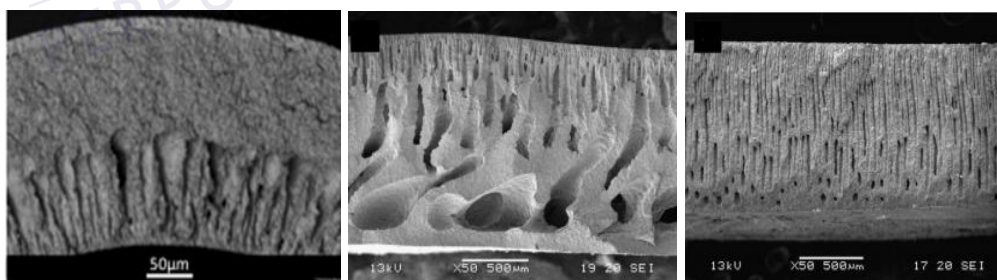
Slip casting



Tape casting



Pressing method



Phase Inversion

Figure 1.1 :Ceramic membrane structure prepared at different techniques

In fabricating ceramic membranes, there are many methods that can be used as tape casting, slip casting, pressing method and extrusion. All of these methods have been established and applied for years. Fabrication of ceramic membranes by these

techniques generally involves multiple steps. Generally, it can be subdivided into three stages: (1) preparation of the ceramic powder paste or suspension, (2) shaping of the ceramic powder into the desired geometry and, (3) heat treatment which including calcination and sintering [15]. After completing these main steps, additional deposition layer or coating layer needs to be formed to allow selective mechanism at the top layer. Then, further heat treatment steps need to be conducted in orders to have a good selectivity as well as to improve other membrane properties. The choice of method for each step depends on the desired membrane configuration, quality, morphology, mechanical, chemical stability and selectivity of the desired final membranes. However, the fabrication method should also be economical and easy to replicate without compromising the quality of final membrane [16].

Phase inversion is a simple technique of membrane fabrication which commonly used in polymeric membranes. The first invention by Loeb and Sourirajan in 1963 is one step technique that able to form asymmetric membrane structure offer a high ability of high flux as well as rejection and selectivity [17]. Recent development of ceramic membrane have shown the implementation of this technique is able to improve gas separation property. As reported, membrane fabrication via phase inversion has promoted a dense top layer with smallest pore size. However, ceramic membrane fabricated via phase inversion so far appear to hold two types of structure: finger-like and sponge-like structure. Figure 1.2 illustrates the structure of membrane that could be obtained by phase inversion. The structure of macrovoids is sometimes observed in ceramic membrane structure. In phase inversion technique, commonly the description of structure always been explained by the concept of ternary diagram, involving three main components: solvent, non-solvent and polymer. However, due to ceramic membranes involve an additional component of ceramic powder, the formation of ceramic membranes can be explained by the viscous fingering mechanism as demonstrated by previous researcher [12, 18]. Viscous fingering is the responsible mechanism that permits the establishment of dense porous structure with certain selectivity. The capability of phase inversion in formation of ceramic membrane lifetime and properties in single step technique has attracted many researchers in developing ceramic membrane especially in gas application.

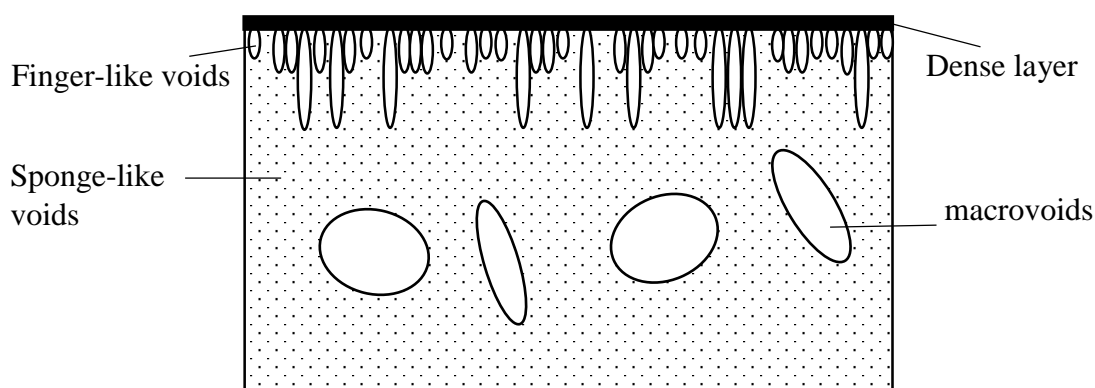


Figure 1.2: Ceramic Membrane Structure fabricated via phase inversion [15]

Ceramic membrane fabricated from phase inversion technique used materials like Alumina, Zirconia and Titania which considered as very expensive materials. Overall comparisons showed that polymeric membranes are still more inexpensive to get compared to ceramic membranes. Even so, a technical and economical comparison between different membrane processes must take into account both investment and maintenance. Investment involves the price of equipment for pretreatment and post treatment of fluids in addition to the monetary value of the membrane plant. Maintenance includes replacement of membranes, electricity consumption, cleaning products and labor prices. Consequently, a comparison of overall costs, including membrane lifetime, cleaning procedures and pretreatment has put a ceramic membrane is a preferable material in a number of applications. More than that, the technical progress made in the manufacture of ceramic membranes with production costs getting closer to those of many polymeric membranes explains why they are entering markets much more extensive than those accessible of the first polymer membranes. In fact, ceramic membrane developed from kaolin and clay has gained attention recently as it employs to offer better properties and at the same time cut off the cost of materials.

1.2 Statement of Problems

Gas separation application seems to be an important research nowadays. This is due to the problem of carbon dioxide emission that could affect severe health. In addition, others gas separation such as oxygen and nitrogen that could be used in medication and production of ammonia, respectively have attracting many researchers in this research.

Membrane for gas separation application have been used in past few years according to the advantages have been promoted. There are two types of membrane which are polymeric and inorganic membrane. However, polymeric membrane has disadvantages which cannot endure high temperature, chemical resistivity and mechanical strength, thus, not suitable for gas application. Due to this, ceramic membrane, a part of inorganic membrane have gaining attention. The combination of high chemical, thermal and mechanical resistance has made ceramic membranes an attractive alternative to polymeric membranes.

In ceramic membrane fabrication process, two most important parameters that always being investigated are materials and fabrication method. For materials, previous study have focused towards refractory ceramic materials such as alumina, nickel and zirconia. These materials are just not requiring high sintering temperature, but expensive too. Due to this, kaolin have become attractive materials to be study in ceramic membrane fabrication. Kaolin is not only cheap, but provides low plasticity and high refractories properties to the membranes [19]. For fabrication methods, pressing method is the one most method that have been used in ceramic membrane fabrication and is well-known method for ceramic membrane. However, pressing method could only produce symmetric membrane structure and need additional method to produce separation layer. Furthermore, pressing method is the most expensive method. Clearly, combining a suitable materials and fabrication method which can cut the time and cost, and hence ceramic membrane price is desirable.

Phase inversion into ceramic membrane fabrication is a promising technique to produce ceramic membrane in a single step at lower cost. It is fast and cost effective technique which hence can promote unique structure (finger-like and sponge-like structure). However, phase inversion in ceramic membrane requiring complex system as many parameters can be involved during fabrication process. Thus the investigation on ceramic membrane fabrication via phase inversion technique was be conducted in this study by study the effect of kaolin particle size, kaolin content and different types of non-solvent coagulant bath.

- [1] US Environmental Protection Agency. Available:
<http://www.epa.gov/climatechange/policy/intensitygoal.html>.
- [2] D. M. D'Alessandro, B. Smit, and J. R. Long, "Carbon Dioxide Capture: Prospects for New Materials," *Angewandte Chemie International Edition*, vol. 49, pp. 6058-6082, 2010.
- [3] A. Brunetti, F. Scura, G. Barbieri, and E. Drioli, "Membrane technologies for CO₂ separation," *Journal of Membrane Science*, vol. 359, pp. 115-125, 2010.
- [4] *Toxicity of carbon dioxide gas exposure, CO₂ poisoning symptoms, carbon dioxide exposure limits*. Available:
<http://www.inspectapedia.com/hazmat/CO2gashaz.thm>
- [5] "IPCC Fourth Assessment Report: Climate Change (AR4)," 2007.
- [6] M. L. Observatory, "Scripps Institution of Oceanography, Atmospheric CO₂ on 5 December 2012," 2012.
- [7] P. Bernardo, E. Drioli, and G. Golemme, "Membrane Gas Separation: A Review/State of the Art," *Industrial & Engineering Chemistry Research*, vol. 48, pp. 4638-4663, 2009.
- [8] T. Isobe, Y. Kameshima, A. Nakajima, K. Okada, and Y. Hotta, "Gas permeability and mechanical properties of porous alumina ceramics with unidirectionally aligned pores," *Journal of the European Ceramic Society*, vol. 27, pp. 53-59, 2007.
- [9] S. Emani, R. Uppaluri, and M. K. Purkait, "Cross flow microfiltration of oil–water emulsions using kaolin based low cost ceramic membranes," *Desalination*, vol. 341, pp. 61-71, 2014.
- [10] B. A. Agana, D. Reeve, and J. D. Orbell, "Performance optimization of a 500 nm TiO₂ ceramic membrane with respect to beverage production wastewater," *Desalination*, vol. 311, pp. 162-172, 2013.

- [11] X. Sui and X. Huang, "The characterization and water purification behavior of gradient ceramic membranes," *Separation and Purification Technology*, vol. 32, pp. 73-79, 2003.
- [12] B. F. K. Kingsbury and K. Li, "A morphological study of ceramic hollow fibre membranes," *Journal of Membrane Science*, vol. 328, pp. 134-140, 2009.
- [13] B. Wang and Z. Lai, "Finger-like voids induced by viscous fingering during phase inversion of alumina/PES/NMP suspensions," *Journal of Membrane Science*, vol. 405–406, pp. 275-283, 2012.
- [14] J. Smid, C. G. Avci, V. Günay, R. A. Terpstra, and J. P. G. M. Van Eijk, "Preparation and characterization of microporous ceramic hollow fibre membranes," *Journal of Membrane Science*, vol. 112, pp. 85-90, 1996.
- [15] K. Li, *Ceramic Membranes for Separation and Reaction*: Wiley, 2007.
- [16] A. Basile, A. Cassano, and N. K. Rastogi, *Advances in Membrane Technologies for Water Treatment: Materials, Processes and Applications*: Elsevier Science, 2015.
- [17] S. Loeb and S. Sourirajan, "Sea Water Demineralization by Means of an Osmotic Membrane," in *Saline Water Conversion?II*. vol. 38, ed: AMERICAN CHEMICAL SOCIETY, 1963, pp. 117-132.
- [18] B. F. K. Kingsbury, Z. Wu, and K. Li, "A morphological study of ceramic hollow fibre membranes: A perspective on multifunctional catalytic membrane reactors," *Catalysis Today*, vol. 156, pp. 306-315, 2010.
- [19] F. Bouzerara, A. Harabi, S. Achour, and A. Larbot, "Porous ceramic supports for membranes prepared from kaolin and doloma mixtures," *Journal of the European Ceramic Society*, vol. 26, pp. 1663-1671, 2006.

- [20] M. Mulder, *Basic Principles of Membrane Technology*: Springer, 1996.
- [21] R. W. Baker, *Membrane Technology and Applications*: Wiley, 2012.
- [22] H. P. Hsieh, *Inorganic Membranes for Separation and Reaction*: Elsevier Science, 1996.
- [23] J. Vital and J. M. Sousa, "1 - Polymeric membranes for membrane reactors," in *Handbook of Membrane Reactors*. vol. 1, A. Basile, Ed., ed: Woodhead Publishing, 2013, pp. 3-41.
- [24] S. Zhou, A. Xue, Y. Zhang, X. Huang, M. Li, Y. Zhao, *et al.*, "Preparation of a new ceramic microfiltration membrane with a separation layer of attapulgite nanofibers," *Materials Letters*, vol. 143, pp. 27-30, 2015.
- [25] K. A. DeFriend, M. R. Wiesner, and A. R. Barron, "Alumina and aluminate ultrafiltration membranes derived from alumina nanoparticles," *Journal of Membrane Science*, vol. 224, pp. 11-28, 2003.
- [26] W. Qin, B. Lei, C. Peng, and J. Wu, "Corrosion resistance of ultra-high purity porous alumina ceramic support," *Materials Letters*, vol. 144, pp. 74-77, 2015.
- [27] Zeman, *Microfiltration and Ultrafiltration: Principles and Applications*: Taylor & Francis, 1996.
- [28] T. Van Gestel, D. Sebold, H. Kruidhof, and H. J. M. Bouwmeester, "ZrO₂ and TiO₂ membranes for nanofiltration and pervaporation," *Journal of Membrane Science*, vol. 318, pp. 413-421, 2008.
- [29] S. Masmoudi, A. Larbot, H. E. Feki, and R. B. Amar, "Elaboration and characterisation of apatite based mineral supports for microfiltration and ultrafiltration membranes," *Ceramics International*, vol. 33, pp. 337-344, 2007.

- [30] J. Fang, G. Qin, W. Wei, and X. Zhao, "Preparation and characterization of tubular supported ceramic microfiltration membranes from fly ash," *Separation and Purification Technology*, vol. 80, pp. 585-591, 2011.
- [31] N. Saffaj, M. Persin, S. A. Younssi, A. Albizane, M. Bouhria, H. Loukili, *et al.*, "Removal of salts and dyes by low $\text{ZnAl}_2\text{O}_4\text{-TiO}_2$ ultrafiltration membrane deposited on support made from raw clay," *Separation and Purification Technology*, vol. 47, pp. 36-42, 2005.
- [32] N. Saffaj, M. Persin, S. A. Younsi, A. Albizane, M. Cretin, and A. Larbot, "Elaboration and characterization of microfiltration and ultrafiltration membranes deposited on raw support prepared from natural Moroccan clay: Application to filtration of solution containing dyes and salts," *Applied Clay Science*, vol. 31, pp. 110-119, 2006.
- [33] M. C. Almandoz, J. Marchese, P. Prádanos, L. Palacio, and A. Hernández, "Preparation and characterization of non-supported microfiltration membranes from aluminosilicates," *Journal of Membrane Science*, vol. 241, pp. 95-103, 2004.
- [34] B. K. Nandi, R. Uppaluri, and M. K. Purkait, "Preparation and characterization of low cost ceramic membranes for micro-filtration applications," *Applied Clay Science*, vol. 42, pp. 102-110, 2008.
- [35] I. Hedfi, N. Hamdi, E. Srasra, and M. A. Rodríguez, "The preparation of micro-porous membrane from a Tunisian kaolin," *Applied Clay Science*, vol. 101, pp. 574-578, 2014.
- [36] A. Belouatek, N. Benderdouche, A. Addou, A. Ouagued, and N. Bettahar, "Preparation of inorganic supports for liquid waste treatment," *Microporous and Mesoporous Materials*, vol. 85, pp. 163-168, 2005.
- [37] I. Ganesh and J. M. F. Ferreira, "Influence of raw material type and of the overall chemical composition on phase formation and sintered microstructure of mullite aggregates," *Ceramics International*, vol. 35, pp. 2007-2015, 2009.

- [38] R. D. Sahnoun and S. Baklouti, "Characterization of flat ceramic membrane supports prepared with kaolin-phosphoric acid-starch," *Applied Clay Science*, vol. 83–84, pp. 399–404, 2013.
- [39] D. Vasanth, G. Pugazhenth, and R. Uppaluri, "Fabrication and properties of low cost ceramic microfiltration membranes for separation of oil and bacteria from its solution," *Journal of Membrane Science*, vol. 379, pp. 154–163, 2011.
- [40] R. Donelson, G. Paul, F. Ciacchi, and S. Badwal, "Permeation and strength characteristics of macroporous supports for gas separation produced by co-sintering mixtures of α -alumina and kaolin," *Journal of Membrane Science*, vol. 463, pp. 126–133, 2014.
- [41] R. Abedini and A. Nezhadmoghadam, "Application of membrane in gas separation processes: Its suitability and mechanisms," *Petroleum & Coal* vol. 52, pp. 69–80, 2010.
- [42] M. B. Choi, D. K. Lim, S. Y. Jeon, H. S. Kim, and S. J. Song, "Oxygen permeation properties of BSCF5582 tubular membrane fabricated by the slip casting method," *Ceramics International*, vol. 38, pp. 1867–1872, 2012.
- [43] M. Barmala, A. Moheb, and R. Emadi, "Applying Taguchi method for optimization of the synthesis condition of nano-porous alumina membrane by slip casting method," *Journal of Alloys and Compounds*, vol. 485, pp. 778–782, 2009.
- [44] N. Miura, Y. Okamoto, J. Tamaki, K. Morinaga, and N. Yamazoe, "Oxygen semipermeability of mixed-conductive oxide thick-film prepared by slip casting," *Solid State Ionics*, vol. 79, pp. 195–200, 1995.
- [45] R. Riedel and I. W. Chen, *Ceramics Science and Technology, Structures*: Wiley, 2011.

- [46] Y. L. Liu and C. Jiao, "Microstructure degradation of an anode/electrolyte interface in SOFC studied by transmission electron microscopy," *Solid State Ionics*, vol. 176, pp. 435-442, 2005.
- [47] T. Isobe, Y. Kameshima, A. Nakajima, K. Okada, and Y. Hotta, "Extrusion method using nylon 66 fibers for the preparation of porous alumina ceramics with oriented pores," *Journal of the European Ceramic Society*, vol. 26, pp. 2213-2217, 2006.
- [48] R. T. Cruz, S. R. Bragança, C. P. Bergmann, T. Graule, and F. Clemens, "Preparation of $\text{Ba}_{0.5}\text{Sr}_{0.5}\text{Co}_{0.8}\text{Fe}_{0.2}\text{O}_{3-\delta}$ (BSCF) feedstocks with different thermoplastic binders and their use in the production of thin tubular membranes by extrusion," *Ceramics International*, vol. 40, pp. 7531-7538, 2014.
- [49] M. Kong, S. Jiang, T. Xie, and H. Zhang, "Low temperature sintering properties of Y-doped BaTiO_3 ceramics by BaB_2O_4 sintering aid," *Microelectronic Engineering*, vol. 86, pp. 2320-2323, 2009.
- [50] Y. Dong, X. Feng, X. Feng, Y. Ding, X. Liu, and G. Meng, "Preparation of low-cost mullite ceramics from natural bauxite and industrial waste fly ash," *Journal of Alloys and Compounds*, vol. 460, pp. 599-606, 2008.
- [51] X. Miao, "Porous mullite ceramics from natural topaz," *Materials Letters*, vol. 38, pp. 167-172, 1999.
- [52] K. Lindqvist and E. Lidén, "Preparation of alumina membranes by tape casting and dip coating," *Journal of the European Ceramic Society*, vol. 17, pp. 359-366, 1997.
- [53] N. Das and H. S. Maiti, "Ceramic membrane by tape casting and sol-gel coating for microfiltration and ultrafiltration application," *Journal of Physics and Chemistry of Solids*, vol. 70, pp. 1395-1400, 2009.

- [54] W. He, H. Huang, J.-f. Gao, L. Winnubst, and C.-s. Chen, "Phase-inversion tape casting and oxygen permeation properties of supported ceramic membranes," *Journal of Membrane Science*, vol. 452, pp. 294-299, 2014.
- [55] B. S. Lalia, V. Kochkodan, R. Hashaiekeh, and N. Hilal, "A review on membrane fabrication: Structure, properties and performance relationship," *Desalination*, vol. 326, pp. 77-95, 2013.
- [56] J. Garcia-Ivars, M.-I. Alcaina-Miranda, M.-I. Iborra-Clar, J.-A. Mendoza-Roca, and L. Pastor-Alcañiz, "Enhancement in hydrophilicity of different polymer phase-inversion ultrafiltration membranes by introducing PEG/Al₂O₃ nanoparticles," *Separation and Purification Technology*, vol. 128, pp. 45-57, 2014.
- [57] M. Sadrzadeh and S. Bhattacharjee, "Rational design of phase inversion membranes by tailoring thermodynamics and kinetics of casting solution using polymer additives," *Journal of Membrane Science*, vol. 441, pp. 31-44, 2013.
- [58] N. Hilal, A. F. Ismail, and C. Wright, *Membrane Fabrication*: CRC Press, 2015.
- [59] J. Barzin and B. Sadatnia, "Correlation between macrovoid formation and the ternary phase diagram for polyethersulfone membranes prepared from two nearly similar solvents," *Journal of Membrane Science*, vol. 325, pp. 92-97, 2008.
- [60] M. H. D. Othman, N. Droushiotis, Z. Wu, G. Kelsall, and K. Li, "Dual-layer hollow fibres with different anode structures for micro-tubular solid oxide fuel cells," *Journal of Power Sources*, vol. 205, pp. 272-280, 2012.
- [61] J. Xiao, C. Xiong, L. Ding, H. Yuan, L. Chen, and W. Liu, "Tubular solid oxide fuel cells fabricated by slip-phase inversion combined with a vacuum-

assisted coating technique," *Ceramics International*, vol. 40, pp. 10163-10169, 2014.

- [62] Z. Wu, R. Faiz, T. Li, B. F. K. Kingsbury, and K. Li, "A controlled sintering process for more permeable ceramic hollow fibre membranes," *Journal of Membrane Science*, vol. 446, pp. 286-293, 2013.
- [63] M. H. D. Othman, Z. Wu, N. Droushiotis, G. Kelsall, and K. Li, "Morphological studies of macrostructure of Ni–CGO anode hollow fibres for intermediate temperature solid oxide fuel cells," *Journal of Membrane Science*, vol. 360, pp. 410-417, 2010.
- [64] L.-Z. Zhang, "Coupled heat and mass transfer through asymmetric porous membranes with finger-like macrovoids structure," *International Journal of Heat and Mass Transfer*, vol. 52, pp. 751-759, 2009.
- [65] N. H. Othman, Z. Wu, and K. Li, "A micro-structured $\text{La}_{0.6}\text{Sr}_{0.4}\text{Co}_{0.2}\text{Fe}_{0.8}\text{O}_{3-\delta}$ hollow fibre membrane reactor for oxidative coupling of methane," *Journal of Membrane Science*, vol. 468, pp. 31-41, 2014.
- [66] Z. Wang, N. Yang, B. Meng, X. Tan, and K. Li, "Preparation and Oxygen Permeation Properties of Highly Asymmetric $\text{La}_{0.6}\text{Sr}_{0.4}\text{Co}_{0.2}\text{Fe}_{0.8}\text{O}_{3-\alpha}$ Perovskite Hollow-Fiber Membranes," *Industrial & Engineering Chemistry Research*, vol. 48, pp. 510-516, 2009.
- [67] M. Lee, B. Wang, Z. Wu, and K. Li, "Formation of micro-channels in ceramic membranes – Spatial structure, simulation, and potential use in water treatment," *Journal of Membrane Science*, vol. 483, pp. 1-14, 2015.
- [68] N. H. Othman, Z. Wu, and K. Li, " $\text{Bi}_{1.5}\text{Y}_{0.3}\text{Sm}_{0.2}\text{O}_{3-\delta}$ -based ceramic hollow fibre membranes for oxygen separation and chemical reactions," *Journal of Membrane Science*, vol. 432, pp. 58-65, 2013.

- [69] Z. Zhong, W. Xing, and B. Zhang, "Fabrication of ceramic membranes with controllable surface roughness and their applications in oil/water separation," *Ceramics International*, vol. 39, pp. 4355-4361, 2013.
- [70] S.-J. Lee, M. Dilaver, P.-K. Park, and J.-H. Kim, "Comparative analysis of fouling characteristics of ceramic and polymeric microfiltration membranes using filtration models," *Journal of Membrane Science*, vol. 432, pp. 97-105, 2013.
- [71] X. Zhang, L. Fan, and F. A. Roddick, "Feedwater coagulation to mitigate the fouling of a ceramic MF membrane caused by soluble algal organic matter," *Separation and Purification Technology*, vol. 133, pp. 221-226, 2014.
- [72] K. C. Khulbe, T. Matsuura, G. Lamarche, and H. J. Kim, "The morphology characterisation and performance of dense PPO membranes for gas separation," *Journal of Membrane Science*, vol. 135, pp. 211-223, 1997.
- [73] J. M. A. Tan and T. Matsuura, "Effect of nonsolvent additive on the surface morphology and the gas separation performance of poly(2,6-dimethyl-1,4-phenylene)oxide membranes," *Journal of Membrane Science*, vol. 160, pp. 7-16, 1999.
- [74] S.-i. Nakao, "Determination of pore size and pore size distribution: 3. Filtration membranes," *Journal of Membrane Science*, vol. 96, pp. 131-165, 1994.
- [75] H. Dzinun, M. H. D. Othman, A. F. Ismail, M. H. Puteh, M. A. Rahman, and J. Jaafar, "Morphological study of co-extruded dual-layer hollow fiber membranes incorporated with different TiO₂ loadings," *Journal of Membrane Science*, vol. 479, pp. 123-131, 2015.
- [76] B. Ghouil, A. Harabi, F. Bouzerara, B. Boudaira, A. Guechi, M. M. Demir, *et al.*, "Development and characterization of tubular composite ceramic

membranes using natural alumino-silicates for microfiltration applications," *Materials Characterization*, 2015.

- [77] Y. Liu, X. Tan, and K. Li, "SrCe_{0.95}Yb_{0.05}O_{3-α} (SCYb) hollow fibre membrane: Preparation, characterization and performance," *Journal of Membrane Science*, vol. 283, pp. 380-385, 2006.
- [78] S. Liu, X. Tan, K. Li, and R. Hughes, "Preparation and characterisation of SrCe_{0.95}Yb_{0.05}O_{2.975} hollow fibre membranes," *Journal of Membrane Science*, vol. 193, pp. 249-260, 2001.
- [79] R. Sarbatly, "Effect of Kaolin/pesf Ratio and Sintering Temperature on Pore Size and Porosity of the Kaolin Membrane Support," *Journal of Applied Sciences*, vol. 11, pp. 2306-2312, 2011.
- [80] J. Fletcher and A. Hill. *Making the connection - particle size, size distribution and rheology*. Available:
<http://www.chemeurope.com/en/whitepapers/61207/making-the-connection-particle-size-size-distribution-and-rheology.html>
- [81] T. J. Fiske, S. B. Railkar, and D. M. Kalyon, "Effects of segregation on the packing of spherical and nonspherical particles," *Powder Technology*, vol. 81, pp. 57-64, 1994.
- [82] Q. Chang, Y. Yang, X. Zhang, Y. Wang, J.-e. Zhou, X. Wang, *et al.*, "Effect of particle size distribution of raw powders on pore size distribution and bending strength of Al₂O₃ microfiltration membrane supports," *Journal of the European Ceramic Society*, vol. 34, pp. 3819-3825, 2014.
- [83] Y. Cai, X. Yin, S. Fan, L. Zhang, L. Cheng, Y. Wang, *et al.*, "Effects of particle sizes and contents of ceramic fillers on tribological behavior of 3D C/C composites," *Ceramics International*, vol. 40, pp. 14029-14037, 2014.

- [84] E. Drioli and L. Giorno, *Comprehensive Membrane Science and Engineering*: Elsevier Science, 2010.
- [85] S. Liu, K. Li, and R. Hughes, "Preparation of porous aluminium oxide (Al₂O₃) hollow fibre membranes by a combined phase-inversion and sintering method," *Ceramics International*, vol. 29, pp. 875-881, 2003.
- [86] J. M. Benito, A. Conesa, F. Rubio, and M. A. Rodríguez, "Preparation and characterization of tubular ceramic membranes for treatment of oil emulsions," *Journal of the European Ceramic Society*, vol. 25, pp. 1895-1903, 2005.
- [87] X. Tan, S. Liu, and K. Li, "Preparation and characterization of inorganic hollow fiber membranes," *Journal of Membrane Science*, vol. 188, pp. 87-95, 6/30/ 2001.
- [88] C. E. Capes, J. C. Williams, and T. Allen, *Particle Size Enlargement*: Elsevier Science, 2013.
- [89] J. Luyten, A. Buekenhoudt, W. Adriansens, J. Coymans, H. Weyten, F. Servaes, *et al.*, "Preparation of LaSrCoFeO_{3-x} membranes," *Solid State Ionics*, vol. 135, pp. 637-642, 2000.
- [90] T.-H. Young and L.-W. Chen, "Pore formation mechanism of membranes from phase inversion process," *Desalination*, vol. 103, pp. 233-247, 1995.
- [91] P. Sukitpaneenit and T.-S. Chung, "Molecular elucidation of morphology and mechanical properties of PVDF hollow fiber membranes from aspects of phase inversion, crystallization and rheology," *Journal of Membrane Science*, vol. 340, pp. 192-205, 2009.
- [92] S. P. Deshmukh and K. Li, "Effect of ethanol composition in water coagulation bath on morphology of PVDF hollow fibre membranes," *Journal of Membrane Science*, vol. 150, pp. 75-85, 1998.

- [93] A. L. Ahmad, W. K. W. Ramli, W. J. N. Fernando, and W. R. W. Daud, "Effect of ethanol concentration in water coagulation bath on pore geometry of PVDF membrane for Membrane Gas Absorption application in CO₂ removal," *Separation and Purification Technology*, vol. 88, pp. 11-18, 3/22/2012.
- [94] R. Rautenbach, R. Rautenbach, and R. Albrecht, *Membrane processes*: Wiley, 1989.
- [95] R. E. Kesting, *Synthetic polymeric membranes: a structural perspective*: Wiley, 1985.
- [96] R. R. Bhave, *Inorganic membranes synthesis, characteristics, and applications*: Van Nostrand Reinhold, 1991.
- [97] R. W. Rice, *Porosity of Ceramics: Properties and Applications*: Taylor & Francis, 1998.
- [98] S. S. Hashim, A. R. Mohamed, and S. Bhatia, "Oxygen separation from air using ceramic-based membrane technology for sustainable fuel production and power generation," *Renewable and Sustainable Energy Reviews*, vol. 15, pp. 1284-1293, 2011.
- [99] Y. Wall, M. Ompe Aime, G. Braun, and G. Brunner, "Gas transport through ceramic membranes under super-critical conditions," *Desalination*, vol. 250, pp. 1056-1059, 2010.
- [100] H. Z. Chen, Z. Thong, P. Li, and T.-S. Chung, "High performance composite hollow fiber membranes for CO₂/H₂ and CO₂/N₂ separation," *International Journal of Hydrogen Energy*, vol. 39, pp. 5043-5053, 2014.
- [101] Z. Zhu, J. Xiao, W. He, T. Wang, Z. Wei, and Y. Dong, "A phase-inversion casting process for preparation of tubular porous alumina ceramic

- membranes," *Journal of the European Ceramic Society*, vol. 35, pp. 3187-3194, 2015.
- [102] C. Hong, A. Dudek, B. Fang, C. Xu, I. W. M. Brown, K. A. Khalil, *et al.*, *Synthesis and Characterization of a Novel Hydrophobic Membrane: Application for Seawater Desalination with Air Gap Membrane Distillation Process*: INTECH Open Access Publisher, 2012.
- [103] A. Larbot, L. Gazagnes, S. Krajewski, M. Bukowska, and K. Wojciech, "Water desalination using ceramic membrane distillation," *Desalination*, vol. 168, pp. 367-372, 2004.
- [104] C. Picard, A. Larbot, E. Tronel-Peyroz, and R. Berjoan, "Characterisation of hydrophilic ceramic membranes modified by fluoroalkylsilanes into hydrophobic membranes," *Solid State Sciences*, vol. 6, pp. 605-612, 2004.
- [105] A. Harabi, F. Zenikheri, B. Boudaira, F. Bouzerara, A. Guechi, and L. Foughali, "A new and economic approach to fabricate resistant porous membrane supports using kaolin and CaCO_3 ," *Journal of the European Ceramic Society*, vol. 34, pp. 1329-1340, 2014.
- [106] S. Khemakhem and R. B. Amar, "Grafting of fluoroalkylsilanes on microfiltration Tunisian clay membrane," *Ceramics International*, vol. 37, pp. 3323-3328, 2011.
- [107] L. Besra, D. K. Sengupta, and S. K. Roy, "Particle characteristics and their influence on dewatering of kaolin, calcite and quartz suspensions," *International Journal of Mineral Processing*, vol. 59, pp. 89-112, 2000.
- [108] R. E. Grim, *Clay Mineralogy*: McGraw-Hill, 1968.
- [109] J. E. Kogel, M. Society for Mining, and Exploration, *Industrial Minerals & Rocks: Commodities, Markets, and Uses*: Society for Mining, Metallurgy, and Exploration, 2006.

- [110] J. Mewis and N. J. Wagner, "Thixotropy," *Advances in Colloid and Interface Science*, vol. 147–148, pp. 214–227, 2009.
- [111] P. Marco, J. Labanda, and J. Llorens, "The effects of some polyelectrolyte chemical compositions on the rheological behaviour of kaolin suspensions," *Powder Technology*, vol. 148, pp. 43–47, 2004.
- [112] H. S. Katz and J. V. Mieski, *Handbook Of Fillers For Plastics*: Springer, 1987.
- [113] T. R. Hull and B. K. Kandola, *Fire Retardancy of Polymers: New Strategies and Mechanisms*: Royal Society of Chemistry, 2009.
- [114] M. Larsson, A. Hill, and J. Duffy, "Suspension Stability: Why Particle Size Zeta Potential and Rheology are Important," *Annual transactions of the nordic rheology society*, vol. 20, pp. 209–214, 2012.
- [115] R. Blazejewski, "Apparent viscosity and settling velocity of suspensions of rigid monosized spheres in Stokes flow," *International Journal of Multiphase Flow*, vol. 39, pp. 179–185, 2012.
- [116] G. Hochgesand, "Rectisol and Purisol," *Industrial & Engineering Chemistry*, vol. 62, pp. 37–43, 1970.
- [117] A. L. Kohl and R. Nielsen, *Gas Purification*: Elsevier Science, 1997.
- [118] B. Su, C. Zhao, and S. Sun, *Polyethersulfone Hollow Fiber Membranes for Hemodialysis*: INTECH Open Access Publisher, 2011.
- [119] Z. Harun, H. S.K., S. Hasan, and M. Z. Yunus, "Effect of thermodynamic properties on porosity of ceramic membrane prepared by phase inversion," *Applied Mechanics and Materials*, vol. 575, pp. 31–35, 2014.
- [120] S. K. Hubadillah, Z. Harun, N. N. Aminudin, and N. Rosman, "Ceramic Membrane Surface Roughness Induced by Modified Phase Inversion: The

effect of Thermodynamic Properties," *Australian Journal of Basic and Applied Sciences*, vol. 8, pp. 233-240, 2014.

- [121] Z. Zhong, D. Li, B. Zhang, and W. Xing, "Membrane surface roughness characterization and its influence on ultrafine particle adhesion," *Separation and Purification Technology*, vol. 90, pp. 140-146, 2012.
- [122] T. R. Albrecht and C. F. Quate, "Atomic resolution imaging of a nonconductor by atomic force microscopy," *J. Appl. Phys.*, vol. 62, pp. 2599-2602, 1987.
- [123] G. Binnig, C. Gerber, E. Stoll, T. R. Albrecht, and C. F. Quate, "Atomic resolution with atomic force microscope," *Surface Science*, vol. 189–190, pp. 1-6, 1987.
- [124] E. Akhondi, F. Wicaksana, W. B. Krantz, and A. G. Fane, "Evaporimetry determination of pore-size distribution and pore fouling of hollow fiber membranes," *Journal of Membrane Science*, vol. 470, pp. 334-345, 2014.
- [125] E. Jakobs and W. J. Koros, "Ceramic membrane characterization via the bubble point technique," *Journal of Membrane Science*, vol. 124, pp. 149-159, 1997.
- [126] F. P. Cuperus, D. Bargeman, and C. A. Smolders, "Permporometry: the determination of the size distribution of active pores in UF membranes," *Journal of Membrane Science*, vol. 71, pp. 57-67, 1992.
- [127] T. Tsuru, T. Hino, T. Yoshioka, and M. Asaeda, "Permporometry characterization of microporous ceramic membranes," *Journal of Membrane Science*, vol. 186, pp. 257-265, 2001.
- [128] M. G. Katz and G. Baruch, "New insights into the structure of microporous membranes obtained using a new pore size evaluation method," *Desalination*, vol. 58, pp. 199-211, 1986.

- [129] F. P. Cuperus, D. Bargeman, and C. A. Smolders, "Characterization of anisotropic UF-membranes: top layer thickness and pore structure," *Journal of Membrane Science*, vol. 61, pp. 73-83, 1991.
- [130] G. Z. Cao, J. Meijerik, H. W. Brinkman, and A. J. Burggraaf, "Permporometry study on the size distribution of active pores in porous ceramic membranes," *Journal of Membrane Science*, vol. 83, pp. 221-235, 1993.
- [131] K. K. Aligizaki, *Pore Structure of Cement-Based Materials: Testing, Interpretation and Requirements*: Taylor & Francis, 2005.
- [132] A. A. Berlin, V. F. Kablov, A. A. Pimerzin, and S. S. Zlotsky, *Key Elements in Polymers for Engineers and Chemists: From Data to Applications*: Apple Academic Press, 2014.
- [133] E. Hara, T. Yokozeki, H. Hatta, Y. Iwahori, and T. Ishikawa, "Comparison of out-of-plane tensile moduli of CFRP laminates obtained by 3-point bending and direct loading tests," *Composites Part A: Applied Science and Manufacturing*, vol. 67, pp. 77-85, 2014.
- [134] C. L. Chapman and E. The University of Texas at Arlington. Biomedical, *Gas Permeation Through Nanoporous Polycarbonate Track-etched Membranes: Pulsed Plasma Polymerization of Thin Coatings to Modulate Gas Permeability*: University of Texas at Arlington, 2007.
- [135] A. Lungu, F. X. Perrin, L. Belec, A. Sarbu, and M. Teodorescu, "Kaolin/poly(acrylic acid) composites as precursors for porous kaolin ceramics," *Applied Clay Science*, vol. 62–63, pp. 63-69, 2012.
- [136] R. Mallada and M. Menéndez, *Inorganic Membranes: Synthesis, Characterization and Applications: Synthesis, Characterization and Applications*: Elsevier Science, 2008.

- [137] F. E. S. A. A. Suryadi Ismadji, *Clay Materials for Environmental Remediation*.
- [138] H. Masuda, K. Higashitani, and H. Yoshida, *Powder Technology: Fundamentals of Particles, Powder Beds, and Particle Generation*: CRC Press, 2006.
- [139] M. Hoch and A. Bandara, "Determination of the adsorption process of tributyltin (TBT) and monobutyltin (MBT) onto kaolinite surface using Fourier transform infrared (FTIR) spectroscopy," *Colloids and Surfaces A: Physicochemical and Engineering Aspects*, vol. 253, pp. 117-124, 2005.
- [140] M. H. B. Hayes, "H.W. van der Marcel and H. Beutelspacher, Atlas of infrared spectroscopy of clay minerals and their admixtures : Elsevier, Amsterdam, 1976, viii+ 396pp., price \$65.95, Dfl. 165.00," *Analytica Chimica Acta*, vol. 99, p. 205, 1978.
- [141] A. Basile, *Handbook of Membrane Reactors: Fundamental Materials Science, Design and Optimisation*: Elsevier Science, 2013.
- [142] S. Liu and K. Li, "Preparation TiO₂/Al₂O₃ composite hollow fibre membranes," *Journal of Membrane Science*, vol. 218, pp. 269-277, 2003.
- [143] J. G. Crespo, K. W. Böddeker, and D. North Atlantic Treaty Organization. Scientific Affairs, *Membrane Processes in Separation and Purification*: Springer, 1994.
- [144] Y. H. Wang, Y. Zhang, X. Liu, and G. Y. Meng, "Microstructure control of ceramic membrane support from corundum-rutile powder mixture," *Powder Technology*, vol. 168, pp. 125-133, 2006.
- [145] J. Zhao, Z. Wang, J. Wang, and S. Wang, "High-performance membranes comprising polyaniline nanoparticles incorporated into polyvinylamine matrix for CO₂/N₂ separation," *Journal of Membrane Science*, vol. 403–404, pp. 203-215, 2012.

- [146] B. Castro-Domínguez, P. Leelachaikul, A. Takagaki, T. Sugawara, R. Kikuchi, and S. T. Oyama, "Perfluorocarbon-based supported liquid membranes for O₂/N₂ separation," *Separation and Purification Technology*, vol. 116, pp. 19-24, 2013.
- [147] H. Strathmann and K. Kock, "The formation mechanism of phase inversion membranes," *Desalination*, vol. 21, pp. 241-255, 1977.
- [148] H. D. Saier, H. Strathmann, and U. V. Mylius, "Mechanism of asymmetric membrane formation," *Angew Makromol. Chem*, vol. 40, pp. 391-404, 1974.
- [149] S. Rafiq, Z. Man, A. Maulud, N. Muhammad, and S. Maitra, "Effect of varying solvents compositions on morphology and gas permeation properties on membranes blends for CO₂ separation from natural gas," *Journal of Membrane Science*, vol. 378, pp. 444-452, 2011.
- [150] M. K. Souhaimi and T. Matsuura, *Membrane Distillation: Principles and Applications*: Elsevier Science, 2011.
- [151] J.-J. Shieh and T. S. Chung, "Effect of liquid-liquid demixing on the membrane morphology, gas permeation, thermal and mechanical properties of cellulose acetate hollow fibers," *Journal of Membrane Science*, vol. 140, pp. 67-79, 1998.
- [152] T. Isobe, Y. Takada, S. Matsushita, and A. Nakajima, "Preparation of AlOOH/Al₂O₃ porous ceramics having CO₂/N₂ gas selectivity of less than 1," *Ceramics International*, 2015.