

CONVECTIVE BOUNDARY LAYER FLOW IN GENERALIZED NEWTONIAN
NANOFLUID UNDER VARIOUS BOUNDARY CONDITIONS

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PTTAUTHM
PERPUSTAKAAN TUN AMINAH

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DEDICATED TO

My beloved father and mother

All this become possible just because of their prayers.

My wonderful wife, NS

*With special gratitude to ARWA the best daughter, I can imagine. you have been a
gift from the beginning.*



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ABSTRACT

Convection heat transfer with the nanofluid plays a vital role in many applications. The four mathematical models of boundary layer flow solved under different boundary conditions. The first problem considered the unsteady squeezing flow of the Carreau nanofluid over the sensor surface, where three different nanoparticles were suspended in the base fluid. A comparison of the results of suspended materials in liquids proved that increased surface permeability leads to increased heat transfer. The second problem described the magnetohydrodynamics (MHD) Darcy-Forchheimer model, which considers Maxwell nanofluids' flow. It was observed that an increase in the Biot number coefficient increased heat transfer. The third problem evaluated activation energy and binary reaction effect on the MHD Carreau nanofluid model. Buongiorno nanofluid model was applied to shear-thinning or pseudoplastic fluid over the pereamble surface. The relationship between the activation energy and chemical reaction is influential and controls heat transfer processes. The fourth problem analyzed the radiative Sutterby model over a stretching/shrinking sheet towards stagnation point flow. Dual solutions were found using the scaling group transformation, which was examined by a stability approach. Such a problem found an increment in the suction parameter, the Deborah number, and the nanoparticle volume fraction delayed the flow separation. The influence of various pertinent parameters on the velocity and temperature distributions has been presented. The most relevant results by the forceful impacts of thermo-physical properties on fluids were analyzed through this work. Modeled equations are based on the conservation laws under the boundary layer approximation. The similarity transformation method is used to convert the governing partial differential equations into ordinary differential equations. They are then solved using a numerical technique, known as the Runge-Kutta-Fehlberg method with shooting technique in the MAPLE 17 or *bvp4c* method in the MATLAB 2019a.

ABSTRAK

Empat model matematik bagi aliran lapisan sempadan pada bendalir Newtonan teritlak telah diselesaikan menggunakan pendekatan separa-analisis tertakluk kepada syarat sempadan yang berlainan. Masalah pertama mempertimbangkan aliran lapisan sempadan nanobendalir Carreau di atas permukaan sensor; tiga nanozarah berlainan telah diletakkan di dalam bendalir asas. Perbandingan keputusan bahan yang direndam di dalam cecair membuktikan bahawa ketelapan permukaan menyebabkan pemindahan haba bertambah. Masalah kedua menggambarkan model Darcy-Forchheimer megnetohidrodinamik (MHD), yang mengambil kira aliran nanobendalir Maxwell dan didapati dengan peningkatan pekali nombor Biot juga meningkatkan pemindahan haba. Masalah ketiga menilai tenaga pengaktifan dan kesan reaksi dedua terhadap model nanobendalir Carreau MHD. Model nanobendalir Buongiorno telah digunakan untuk bendalir penipisan ricih atau bendalir pseudoplastik atas permukaan sedutan/semburan. Begitu juga hubungan di antara tenaga pengaktifan dengan reaksi kimia yang mempengaruhi dan mengawal proses pemindahan haba. Masalah keempat menganalisis model radiasi Sutterby atas helaian telap yang meregang/mengecut terhadap aliran titik genangan dalam nanobendalir. Penyelesaian dual telah diperoleh menggunakan penjelmaan kumpulan penskalaan dan dikaji dengan pendekatan kestabilan. Didapati dengan penambahan parameter sedutan, nombor Deborah, dan pecahan isipadu nanozarah telah melambatkan pemisahan aliran. Pengaruh pelbagai parameter penting ke atas halaju dan taburan suhu digambarkan secara bergraf dan jadual serta dibincangkan. Persamaan-persamaan yang dimodelkan adalah berasaskan kepada hukum-hukum keabadian tertakluk kepada penghampiran lapisan sempadan. Kaedah penjelmaan keserupaan telah digunakan untuk menukar persamaan menakluk kepada persamaan terbitan biasa. Ia kemudian diselesaikan secara penyelesaian berangka, iaitu kaedah Runge-Kutta Fehlberg dengan teknik tembakan menggunakan MAPLE 17 atau kaedah bvp4c di MATLAB 2019a.

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LIST OF SYMBOLS AND ABBREVIATIONS

| | | |
|-------------|---|---|
| A_I | - | First order Rivlin-Erickson (deformation rate tensor) |
| Al_2O_3 | - | Aluminium oxide |
| b | - | Squeezed flow parameter |
| B_o | - | Magnetic field strength |
| Bi | - | Biot number |
| c | - | Constant |
| c_p | - | Specific heat capacity at constant pressure |
| C | - | Nanoparticle concentration |
| C_w | - | Nanoparticle concentration at the wall |
| C_∞ | - | Ambient nanoparticle concentration |
| C_A | - | Nanoparticle concentration of A case reaction |
| C_b | - | Drag coefficient |
| C_{fx} | - | Skin friction coefficient |
| C_B | - | Diffusion parameter $C_B = D_B / T$ |
| C_T | - | Diffusion parameter $C_T = D_T / \phi$ |
| Cu | - | Copper |
| D_B | - | Brownian diffusion coefficient |
| D_b | - | Diffusion coefficient |
| D_T | - | Thermophoretic diffusion |
| De | - | Deborah number |
| $\phi(s')$ | - | Error for guess s' for initial condition |
| $\phi(s^*)$ | - | Error for guess s^* for initial condition |
| E | - | Activation energy parameter |
| E_a | - | Activation energy |
| Ec | - | Eckert number |

| | | |
|-------------|---|--|
| f | - | Dimensionless stream function |
| F | - | Non-uniform inertia coefficient of the porous medium |
| Fe_3O_4 | - | Magnetite nanoparticles |
| Fr | - | Inertia coefficient (Forchheimer number) |
| G | - | Generalized parameter of the scaling group |
| $h(t)$ | - | Highest squeezed channel |
| h_o | - | Constant |
| h_w | - | Heat transfer coefficient at the wall |
| h_m | - | Convection mass transfer coefficient |
| H | - | Fitted rate constant |
| I | - | Identity tensor |
| j | - | Mass flux of nanoparticle |
| k | - | Thermal conductivity |
| k_B | - | Boltzmann constant |
| k_l | - | Rosseland mean absorption |
| K | - | Permeability of porous medium |
| K_r^2 | - | Binary chemical reaction rate |
| l | - | Characteristic shape of nanoparticle |
| L | - | Characteristic length scale |
| M | - | Magnetic field parameter |
| n | - | Power law index parameter |
| \check{n} | - | Normal unit vector at a point |
| N_b | - | Brownian motion parameter |
| N_t | - | Thermophoresis parameter |
| Nu | - | Nusselt number |
| Nu_x | - | Local Nusselt number |
| N_A'' | - | Mass flux of reaction A |
| P | - | Pressure |
| Pr | - | Prandtl number |
| $q(x)$ | - | Heat flux of the wall |
| q''_w | - | Surface heat flux |
| Rd | - | Radiation parameter |

| | | |
|------------------------|---|--|
| Re | - | Reynolds number |
| Re_x | - | Local Reynold number |
| s | - | Permeable velocity parameter |
| s', s^* | - | guesses for unknown initial conditions |
| S | - | Extra stress tensor |
| Sc | - | Schmidt number parameter |
| Sh_x | - | Sharwood number parameter |
| t | - | Time |
| t^* | - | guess value |
| T | - | Temperature of the fluid |
| \mathbf{T} | - | Cauchy stress tensor |
| T_o | - | Reference temperature |
| T_w | - | Temperature at the wall |
| T_∞ | - | Temperature at the stream flow |
| $T(y)$ | - | Temperature gradient in y -directions |
| $tr(A_l^2)$ | - | Trace of matrix A_l^2 |
| u, v | - | Velocity components in x, y directions, respectively |
| u_l, v_l | - | reference velocity components in x, y directions, respectively |
| \bar{u}, \bar{v} | - | Velocity vector components in \bar{x}, \bar{y} -directions |
| u_o | - | Characteristic velocity vector component |
| \bar{u}_w, \bar{v}_w | - | Velocity vector component at the wall |
| \bar{u}_e | - | Free stream velocity vector component |
| U_∞ | - | Uniform velocity of the free stream flow |
| U_w | - | Uniform velocity of the free stream flow |
| $u(y)$ | - | Velocity gradient in y -directions |
| $U(x)$ | - | Uniform velocity of the free stream flow |
| V | - | Characteristic velocity of the flow |
| We | - | Weissenberg number |
| ω_i | - | Constant to be determined in which $i=1\dots,8$ |

| | | |
|--|---|--|
| α | - | Thermal diffusivity |
| α', β' | - | Two-point boundary conditions values |
| $\dot{\gamma}$ | - | The rate of shear stress |
| γ | - | Eigenvalue parameter |
| δ | - | Boundary layer thickness |
| δ_t | - | Thermal boundary layer thickness |
| δ_c | - | Concentration boundary layer thickness |
| δ_1 | - | Temperature difference parameter |
| ε | - | Stretching/shrinking |
| ϵ | - | Small quantity constant |
| η | - | Similarity variable |
| θ | - | Dimensionless temperature |
| $-\theta'(0)$ | - | The rate of heat transfer |
| κ | - | Binary reaction parameter |
| λ | - | Porosity parameter of porous medium |
| μ | - | Dynamic viscosity |
| μ_∞ | - | Viscosity of infinite shear rate |
| μ_o | - | Low shear rate viscosity |
| ν | - | Kinematic viscosity |
| ρ | - | Density of fluid |
| ρc_p | - | Heat capacity |
| σ^{**} | - | Stefan-Boltzmann constant |
| σ | - | Electrical conductivity |
| $\tau_{xy}, \tau_{yx}, \tau_{xx}, \tau_{yy}$ | - | momentum components shear stresses |
| τ | - | Similarity transformation for time |
| τ_w | - | Shear stress at the wall |
| φ | - | Dimensionless concentration |
| ϕ | - | Nanoparticle volume fraction |
| ψ | - | Stream function |
| Γ | - | Material time constant |
| γ | - | Nanoparticle volume fraction parameter |

Subscript

| | | |
|-----------|---|-----------------------------|
| <i>bf</i> | - | Fluid |
| <i>nf</i> | - | Nanofluid |
| <i>s</i> | - | Nanoparticle |
| <i>p</i> | - | Particle |
| <i>w</i> | - | Surface |
| ∞ | - | Infinity (free stream flow) |

Superscripts

| | | |
|---|---|---------------------|
| T | - | Transpose of matrix |
|---|---|---------------------|

Abbreviations

| | | |
|---------------|---|---|
| BVP | - | Boundary value problem |
| bvp4c | - | Boundary value problem with fourth-order accuracy |
| IVP | - | Initial value problem |
| MHD | - | Magnetohydrodynamic |
| <i>MWCNTs</i> | - | Multi-walled carbon nanotubes |
| ODEs | - | Ordinary differential equations |
| PDEs | - | Partial differential equations |
| <i>SWCNTs</i> | - | Single-walled carbon nanotubes |
| 2D | - | Two-dimensional |

LIST OF APPENDICES

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CHAPTER 1

INTRODUCTION

1.1 Background of the study

The theoretical investigation of the flow of generalized Newtonian fluid or non-Newtonian fluids continues to receive special status in the literature due to the growing importance of such fluid in modern technology and industries. The flows of generalized Newtonian fluids occur in many applications, with important examples in industrial processes that involve synthetic fibers, extrusion of molten plastic, flows of polymer solutions, bioengineering and heat exchange efficiency (Rieutord, 2014). Simple examples of generalized Newtonian fluids are slurries, pastes, polymer solutions, multigrade engine oils, toothpaste, liquid soaps and peanut. The main distinguishing feature of many generalized Newtonian fluids is that they exhibit both viscous and elastic properties. Note that shear stress depends only on the shear rate, while the relation between shear stress and the shear rate depends on time (Schowalter, 1978).

These fluids exhibit numerous strange features, for example, shear-thinning or thickening and display of elastic effects. Hence, the classical Navier-Stokes equations are not appropriate in describing their rheological behavior. Due to the large difference in the chemical and physical structure of generalized Newtonian fluids and the variation of flows, the usual Navier Stokes equations may fail. They cannot represent all the rheological properties of generalized Newtonian fluids. Thus, many mathematical models have been proposed to describe these fluids' physical behavior, such as Carreau fluid, Maxwell fluid, and Sutterby fluid. Unlike viscous

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