

## COD AND AMMONIA REMOVAL FROM LANDFILL LEACHATE USING MIXED GRANULAR ADSORBENT MEDIA

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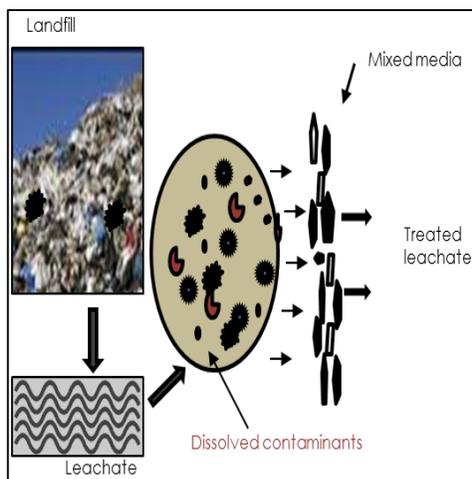
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### Graphical abstract



### Abstract

Landfills generate leachate that contains elevated concentration of contaminants and is hazardous to human health and the ecosystem. In this study, the mixture of granular feldspar and cockle shells was investigated for remediation of COD and ammonia from landfill leachate. All adsorbent media were sieved to a particle size between 2.00 and 3.35 mm. The results revealed that the optimum mixing ratio of feldspar and cockle shells was 20:20, shaking speed was 150 rpm, pH level was 6, shaking time was 120 min, and dosage was 30 g. The adsorption isotherm analysis reveals that the Langmuir isotherm yielded the best fit to experimental data as compared to the Freundlich isotherm. The media produce encouraging results and can potentially be used as a good and sustainable adsorbent.

Keywords: Cockle shells, feldspar, COD, ammonia nitrogen, leachate

### Abstrak

Tapak pelupusan menjana larut resapan yang mengandungi kepekatan bahan pencemar yang tinggi dan berbahaya kepada kesihatan manusia dan ekosistem. Dalam kajian ini, campuran butiran yang terdiri daripada feldspar dan kulit kerang dikaji bagi pengurangan COD dan ammonia dari larut resapan di tapak pelupusan. Kesemua media penjerap disaring kepada saiz partikel di antara 2.00 dan 3.35 mm. Hasil kajian menunjukkan bahawa campuran nisbah optimum feldspar dan kulit kerang adalah 20:20, kelajuan goncangan 150 rpm, pH 6, masa goncangan 120 min dan dosej sebanyak 30 g. Daripada analisis isoterma penjerapan mendedahkan isoterma Langmuir adalah lebih sepadan dengan data ujikaji berbanding isoterma Freundlich. Media penjerap yang dihasilkan memberi keputusan yang memberangsangkan dan berpotensi digunakan sebagai penjerap yang baik dan mampan.

Kata kunci: Kulit kerang, feldspar, COD, ammonia, larut resapan

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## 1.0 INTRODUCTION

Malaysia has an increasing problem of solid waste disposal, in which a large number of land disposal sites do not have sufficient or comprehensive facilities to adequately handle the ever-increasing waste generation and consequent leachate formation. Paradoxically, the main hazard to the environment from landfills that receive solid waste originates as a liquid. Diverse leachates are produced from the organic dissolution and densification of wet refuse, but the majority is produced by infiltration from precipitation, evaporation, surface runoff, and storage capacity. Infiltration primarily occurs during the landfill operational life, but the water may also enter in lesser amounts after closure due to leakage through the cap. This leachate (liquid) percolates in the landfill for several years, interacting with paints and spent petroleum products, pesticides, and a multitude of other items that contribute to making up the landfill. Aerobic and anaerobic degradation also occur under suitable conditions within the landfill. Leachate constitutes dissolved contaminants, volatile organic acids, toxic heavy elements, and high concentrations of chemical oxygen demand (COD) and ammonia [1–8]. When leachate containing high levels of dissolved contaminants is inadvertently discharged into the environment, it can contaminate the soil and water bodies, seriously threatening the environment and public health (9, 10). One of the sources of groundwater pollution is landfill leachate, which is also a major environmental concern at sanitary landfills that demands extensive controlling measures.

Leachate treatment imposes technical and economic challenges to water quality managers. Many landfill leachate treatments that apply the conventional approach involve high-technology processes. High-technology methods generate residues and are saddled with high initial and long-term operational expenditure as well as low applicability to many types of pollutants to achieve discharge standards [11, 12]. At present, an increasing amount of research involving the possible application of alternative adsorbents (10) to obtain appropriate leachate treatment or as a substitute approach to conventional media for the treatment of pollutants that exist in wastewater. Feldspar (F), which was successfully applied in the removal of heavy metals from industrial wastewater, is a promising adsorbent (10). Meanwhile, cockle shell (CS) is hydrophobic and primarily comprises CaO of nearly equal percentage ratio (96.28%) as compared to that in limestone (97.67%). Apart from being environmentally friendly, CS can be used for the removal of organic and inorganic pollutants in wastewater [13–15]. Furthermore, considerable research has investigated the use of conventional media involving a combination of activated carbon and zeolite for leachate remediation; however, attention on the application of alternative media as a substitute for

conventional media in landfill leachate treatment is emerging [16–19]. The present article introduces the research results on leachate treatment using alternative biomed. Batch experiments using combined loose media of CS and zeolite were conducted using one-factor-at-a-time optimization to determine the best ratio of adsorbents for COD and ammonia removal at ambient temperature, as well as the most effective conditions with respect to adsorbent dosage, pH, agitation speed, and contact time on the adsorbent.

## 2.0 METHODOLOGY

Leachate sample was collected at Simpang Renggam municipal landfill in Johor. Raw leachate was collected from the inlet of the detention pond using clean 20 L high-density polyethylene plastic containers. Then, leachate was characterized within 24 h according to the standard methods for the examination of water and wastewater [18–21]. Two different mixed media types (F and CS) were then used for the experiments. F and CS were cleaned according to Daud (14) and sieved to obtain particle sizes between 2.00 and 2.35 mm. The determination of the optimum condition of shaking speed and time experiments was conducted in a series of 250 mL conical flasks containing 100 mL of raw leachate and some measured quantity by mass (equivalent to 40cm<sup>3</sup>) of the mixed media by respectively varying the shaking speed and time. The influence of pH on COD and ammonia remediation was determined by varying the pH levels to 4, 6, 7, 8, and 9. The pH variation was carried out with 97% H<sub>2</sub>SO<sub>4</sub> and 1 M NaOH. Furthermore, optimum dosage was determined by varying the adsorbent dose from 4 g to 56 g. The sequence of media mixing ratios for F:CS were 8:56, 16:48, 25:40, 33:32, 41:24, 50:16, and 58:8, which is based on mass (g) (19,11). Finally, the optimum values of the combination of the two media were obtained by plotting mixing ratio against removal percentages of COD and ammonia.

## 3.0 RESULTS AND DISCUSSION

### 3.1 Media Mix Ratio

The percent removal of COD and ammonia nitrogen in the sample after mixing of feldspar with CS was analysed. The results show that the most favourable conditions occurred for COD and ammonia removal at 20:20 mix ratio which corresponds to 30% and 24% removal respectively for COD and ammonia by the media (Figure 1). The ratio 20:20 also represent about 50% replacement of the conventional media.

A one-tailed two-sample t-test was also used to ascertain whether the mix ratio of 20:20 removes more of the parameters compared to the generality of the

mix ratios. The t-test results for 20:20 mix ratio was summarized in Table 1.

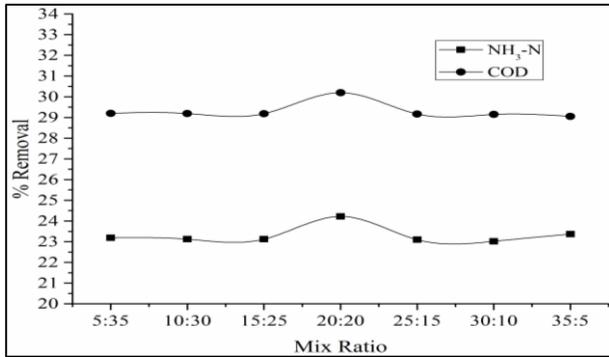


Figure 1 Mix ratio of adsorbents for COD and NH<sub>3</sub>-N removal

The results show that on average, the mix ratio 20:20 removed more of the COD and ammonia in comparison to the general mix ratios. The results also revealed that a significant difference exists for the 20:20 mix ratio data. It is also evident from data that statistically, mix ratio 20:20 is significant in removal as compared to the overall mix ratios.

Table 1 t-Test result

Parameter	N	mean	All mix ratio mean	T-value	P-value
NH <sub>3</sub> -N	7	24.22	23.3045	-5.798	<0.001
COD	7	30.19	29.3037	-5.953	<0.001

### 3.2 Shaking Speed

The optimum media mixing ratio of 20:20 was employed to determine the optimum shaking speed based on COD and ammonia removal. The percentage of COD and NH<sub>3</sub>-N decreased with the increase in agitation rate from 50 to 150 rpm. The result show that removal increased substantially from 50 up to 150 there after it decreased (Figure 2). The optimum shaking speed adopted for further experiment was 150 rpm. This shaking speed corresponds to COD and NH<sub>3</sub>-N removal rates of 40% and 30% respectively.

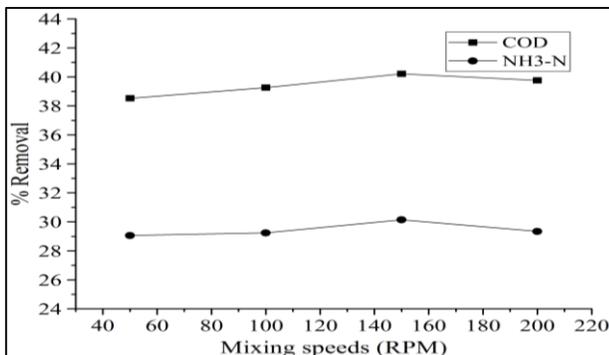


Figure 2 Mixing speeds of media for COD and NH<sub>3</sub>-N removal

### 3.3 pH

pH is important for the determination of optimum parameters (18). The influence of pH on the removal of COD and ammonia was investigated by varying the pH of the solution between 2 and 9.

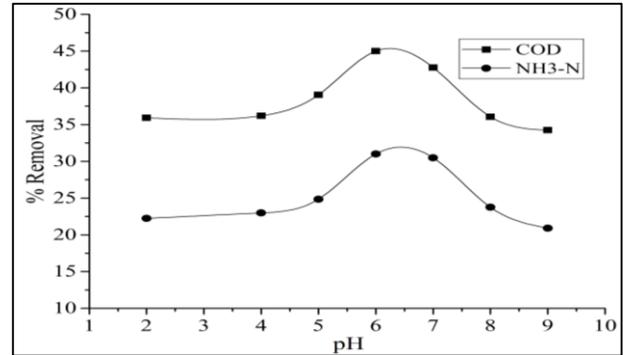


Figure 3 Optimum pH for COD and NH<sub>3</sub>-N removal

The results revealed that the removal rate was enhanced with the increase in pH until the pH reached 6, and then steadily decreased until the pH reached 9. An optimum removal rate of 45% and 31% for COD and ammonia was achieved at pH 6 (Figure 3).

### 3.4 Contact Time

The concentration of adsorbate species in the bulk fluid and the interaction time between the adsorbent and adsorbate play dominant roles in minimizing pollutants from effluent water. The shaking time for COD and ammonia nitrogen removal by the adsorbent illustrated that the removal of COD was increasing with the increment in time (see figure 4) and attained equilibrium in about 120 min. Similarly, ammonia nitrogen removal was found to be 120 min. The shaking time of 120 min was adopted, for COD and ammonia nitrogen removal which corresponds to 55% and 39% respectively.

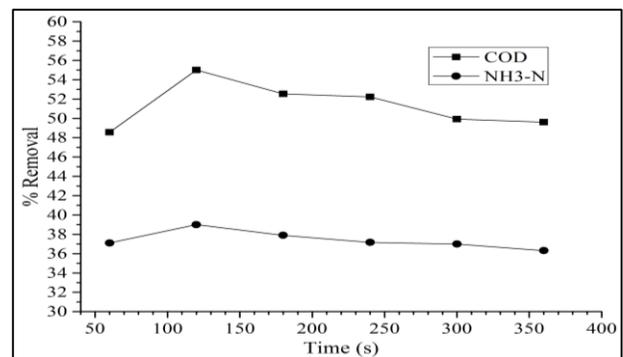


Figure 4 Optimum shaking time for COD and NH<sub>3</sub>-N removal

### 3.5 Dosage of Media

Inadequate dosage or excess dosage of media may lead to an inadequate capacity in parameter removal.

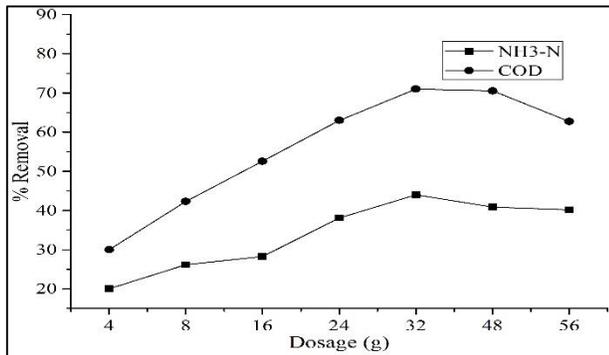


Figure 5 Optimum dosage for COD and NH<sub>3</sub>-N removal

The effect of adsorbent concentration on adsorption of COD and ammonia was determined by varying the dosage in the range of 4–56 g using predetermined optimum conditions (mixed ratio of 20:20, shaking speed of 150 rpm, pH level of 6, and shaking time of 120 min).

From the results, the percentage removal of the adsorbate increased with the increase in the adsorbent dose until 32g dosage was reached (Figure 5). At this dosage, the COD and ammonia nitrogen removal rates was 71% and 44% respectively. This behaviour can be credited to an increase in the amount of available sorption sites from the onset until the optimum mass is reached, any further increase in the adsorbent dose results in aggregation, which can decrease the chances of occurrence for available sorption sites for the molecules.

### 3.6 Adsorption Isotherms

The determination of the adsorption isotherms is important for the optimization of sorption experiments. The two well-known adsorption isotherms (Langmuir and Freundlich) have been used for this study. The Langmuir isotherm analyzes the formation of a monolayer adsorbate onto the adsorbent surface. On the other hand, the Freundlich isotherm model explains heterogeneous surface adsorption, in which the surface concentration of the adsorbate on the adsorbent increases with the elevation in the initial concentration of the solution. The correlation coefficients R<sup>2</sup> demonstrate or differentiate suitability of each equation.

Table 2 Coefficients of Langmuir isotherm models for COD and NH<sub>3</sub>-N uptake by the media

	Langmuir constant		
	q <sub>m</sub>	K <sub>L</sub>	R <sup>2</sup>
COD	40.81	0.0959	0.8861
NH <sub>3</sub> -N	-987.87	4.4343	0.7549

Table 3 Coefficients of Freundlich isotherm models for COD and NH<sub>3</sub>-N uptake by the media

	Freundlich constant		
	logK <sub>f</sub>	1/n	R <sup>2</sup>
COD	0.3784	0.2788	0.7461
NH <sub>3</sub> -N	-1.513	3.7189	0.8814

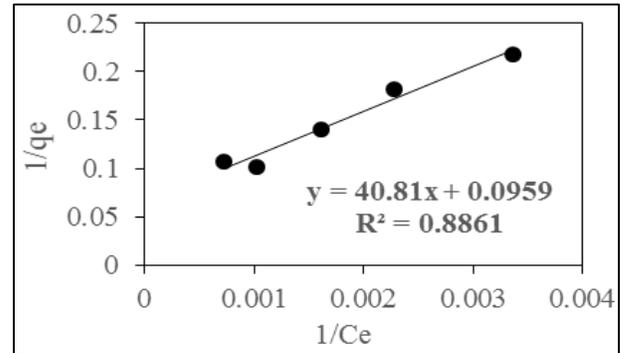


Figure 6 Langmuir Isotherm for COD adsorption

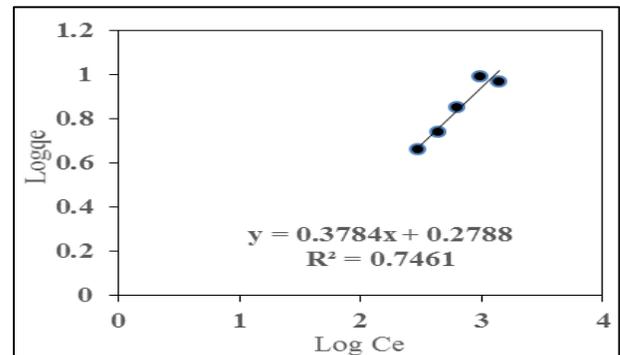


Figure 7 Freundlich Isotherm for COD adsorption

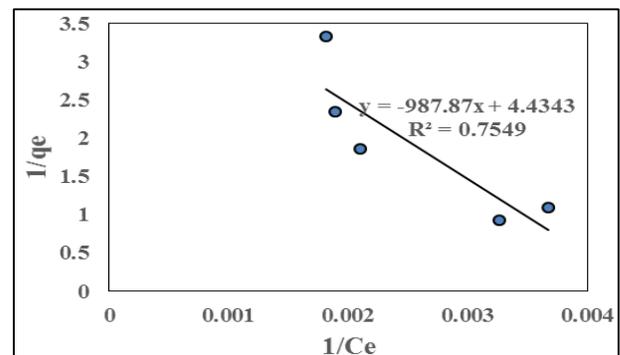
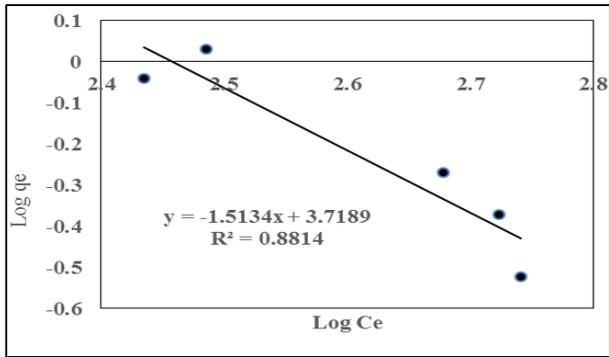


Figure 8 Langmuir Isotherm for NH<sub>3</sub>-N adsorption



**Figure 9** Freundlich Isotherm for NH<sub>3</sub>-N adsorption

The correlation value obtained for the Langmuir and Freundlich equations for COD shows that the value of R<sup>2</sup> was higher in Langmuir than in Freundlich. Similarly, the R<sup>2</sup> values for NH<sub>3</sub>-N were higher in Freundlich (see Table 2 and 3). This finding indicates that the Langmuir isotherm model is more suitable than Freundlich isotherm for evaluating the adsorption equilibrium required for COD, implying monolayer formation while Freundlich was favourable in ammonia uptake by the media, which also indicates heterogeneous surface adsorption. The fitting of the Langmuir isotherm for COD by similar adsorbents was also reported in another study by Siti *et al.* (22) and Daud (23).

#### 4.0 CONCLUSION

The effectiveness of the mixture of CS and F as adsorbents was determined for the removal of ammoniacal nitrogen and COD from a landfill leachate. The pertinent parameters of mixing ratio, shaking speed, shaking time, pH, and adsorbent dose that define the optimum conditions were determined as follows: mixing ratio of 20:20, shaking speed of 150 rpm, pH level of 6, shaking time of 120 min, and dosage of 30 g. The adsorption isotherm analysis reveals that both Langmuir and Freundlich isotherms fit the experimental data. The media can be used as an economical adsorbent for stabilized landfill effluent treatment. Furthermore, investigation is being performed to ascertain other aspects like desorption as well as disposal of used up adsorbents that may influence the research area.

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